

SOLKANE® - INFORMATION SERVICE

Solkane® 410 Thermodynamics

SOLVAY FLUOR

Technical Service - Refrigerants -

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1 Units and Symbols

Symbol	Unit	Meaning/Definition
A, B	[-]	Parameters of the Wagner equation
C	[-]	Parameter of the equation for density of boiling liquid
D	[kJ/(kg K)]	Parameter of the equation for specific heat capacity in an ideal gas state
E, F, G	[-]	Parameter of the Martin-Hou equation
H	[Pa s/K]	Parameter of the equation for dynamic viscosity of vapour
J	[W/(m K)]	Parameter of the equation for thermal conductivity of the saturated liquid
K	[W/(m K)]	Parameter of the equation for thermal conductivity of the saturated vapour
L	[N/(m K)]	Parameter of the equation for surface tension
M	[kJ/(kg K)]	Parameter of the equation for specific heat capacity of the saturated liquid
R	[bar m ³ /(kg K)]	Gas constant
T	[K]	Temperature
b	[m ³ /kg]	Parameter of the Martin-Hou equation
c	[kJ/(kg K)]	Specific heat capacity
e	[kJ/kg]	Specific exergy
h	[kJ/kg]	Specific enthalpy
k	[-]	Parameter of the Martin-Hou equation
p	[bar]	Pressure
r	[kJ/kg]	Enthalpy of vaporization
s	[kJ/(kg K)]	Specific entropy
t	[°C]	Temperature
v	[m ³ /kg]	Specific volume
η	[Pa s]	Dynamic viscosity
λ	[W/(m K)]	Thermal conductivity
ρ	[kg/m ³]	Density
σ	[N/m]	Surface tension

Indices

'	Liquid
''	Vapour
<i>c</i>	Critical value
<i>r</i>	Reduced value
<i>i</i>	Run index
<i>u</i>	Ambient conditions
<i>p</i>	Isobar
<i>v</i>	Isochor
<i>0</i>	Ideal gas

2 Introduction

The refrigerant Solkane®410 is a long-term replacement for applications, where a compact design and a high energy efficiency shall be realised. Solkane®410 replaces R22 and also R13B1.

The ozone depletion potential of the hydrochlorofluorocarbon (HCFC) R22 is reduced to a fraction of the ODPs of chlorofluorocarbons (CFCs). R22 is therefore regarded as an intermediate solution. The use of HCFCs will be gradually reduced and these products will finally be banned. By 2030 the production of HCFCs will be phased out in developed countries¹. Accelerated phase out scenarios may apply in selected countries especially in Europe.

Solkane®410 is a near azeotropic blend of R32 and R125 (50 /50 weight-%). Both components are partly halogenated hydrofluorocarbons, containing only carbon, fluorine and hydrogen. They do not contribute to the depletion of the stratospheric ozone layer.

Due to the minimal temperature glide (<0.2K) Solkane®410 can be treated as a pure fluid for technical applications. Compared to R22 Solkane®410 has a significant higher volumetric capacity.

Solkane®410 is non-flammable. Its toxicity is low and comparable to the toxicity of R22.

The pressure level of Solkane®410 higher is than that of R22.

Solkane®410 is therefore unsuitable for the retrofit of existing R22-units. R13B1-units can be adapted to the use with Solkane®410.

¹ In the sense of Montreal Protocol (1995 Vienna meeting)

3 Thermophysical Properties

3.1 Physical Data

Chemical name	[-]	Difluoromethane/ Pentafluoroethane/
Chemical formula	[-]	CH ₂ F ₂ /CF ₃ CHF ₂
CAS No.	[-]	75-10-5/354-33-6
Molecular weight	[kg/kmol]	72.6
Boiling point	[°C]	-51.5
Critical temperature	[°C]	70.2
Critical pressure	[bar]	47.7
Saturated liquid density ²	[kg/m ³]	1061
Saturated vapour density ²	[kg/m ³]	65.56
Vapour pressure ²	[bar]	16.47
Enthalpy of vaporization ¹	[kJ/kg]	271.63
Liquid thermal conductivity ²	[W/m K]	87.249E-3
Vapour thermal conductivity ²	[W/m K]	16.532E-3
Surface tension of liquid ²	[N/m]	5.158E-3
Specific heat capacity of liquid ²	[kJ/(kg K)]	1.692
Specific heat capacity of vapour ¹	[kJ/(kg K)]	1.346
Liquid viscosity ²	[Pa s]	0.1217E-3
Flammability limit in air ³	[Vol.-%]	None ³

¹ at 1.013 bar

² at 25°C and saturated conditions

³ according to DIN 51649 and UL 2128

3.2 Basis of Thermodynamic Calculation

The thermodynamic calculation equations have been adapted to ISO/DIS 17584, as at 12/2003. They fulfil this standard with the exception of the thermal capacities in a saturated state of $0.59 < T_R < 0.94$ and in an overheated state of $0.5\text{MPa} < p < 0.5\text{MPa}$ and $T_{\text{max}} = 440\text{K}$.

The Wagner equation

$$\ln p_R = (A_1(1-T_R) + A_2(1-T_R)^{B_1} + A_3(1-T_R)^{B_2} + A_4(1-T_R)^{B_3} + A_5(1-T_R)^{B_4} + A_6)/T_R \quad (1)$$

where $T_R = \frac{T}{T_c}$ and $p_R = \frac{p}{p_c}$

was chosen to describe the vapour pressure. The constants and values for the critical pressure p_c and the critical temperature T_c are as follows:

	Bubble Pressure	Dew Pressure
A_1 [-]	-7.6368778	-7.70876155
A_2 [-]	3.020664659	3.293380929
A_3 [-]	-6.02265976	-6.477671
A_4 [-]	9.747548052	10.23405674
A_5 [-]	-8.74776593	-9.01987639
A_6 [-]	0.002434753	0.001688002
B_1 [-]	1.5	1.5
B_2 [-]	2	2
B_3 [-]	2.5	2.5
B_4 [-]	3	3
T_c [K]	343.315	
p_c [bar]	47.6985	

A slight difference between dew- and vapour pressure for Solkane®410 do exists. The difference is smaller than 0.02 bar and is therefore classified as insignificant for technical purposes.

The density of the boiling liquid is described by the equation

$$\rho'_R = 1 + C_1(1-T_R)^{1/3} + C_2(1-T_R)^{2/3} + C_3(1-T_R) + C_4(1-T_R)^{4/3} \quad (2)$$

where $\rho'_R = \frac{\rho'}{\rho_c}$.

The constants and the value for the critical density are:

C_1 [-]	1.239281254	C_4 [-]	0.310613093
C_2 [-]	1.206550532	ρ_c [kg/m ³]	551.89
C_3 [-]	-0.31471863		

The specific heat capacity under ideal gas conditions is represented by the equation

$$c_p^0 = D_1 + D_2T + D_3T^2 + D_4T^3 + D_5/T \quad (3)$$

The coefficients are:

D_1	[kJ/(kg K)]	8.38141E-01	D_4	[kJ/(kg K ³)]	-7.96710E-09
D_2	[kJ/(kg K ²)]	-1.62958E-03	D_5	[kJ/kg]	-2.45256E+01
D_3	[kJ/kg]	8.40584E-06			

The equation of state according to Martin-Hou is

$$p = \frac{RT}{z} + \frac{E_1 + F_1T + G_1e^{-kT_R}}{z^2} + \frac{E_2 + F_2T + G_2e^{-kT_R}}{z^3} + \frac{E_3}{z^4} + \frac{E_4 + F_4T + G_4e^{-kT_R}}{z^5} \quad (4)$$

and is a good representation of the $p\nu T$ relationship for Solkane®410. The coefficients of the equation are:

E_1	[-]	-1.89512E-03	F_2	[-]	9.56704E-10
E_2	[-]	2.15923E-07	F_4	[-]	3.61296E-14
E_3	[-]	-1.87075E-10	G_1	[-]	-4.25660E-02
E_4	[-]	-1.59054E-11	G_2	[-]	-3.20769E-06
F_1	[-]	3.22638E-06	G_4	[-]	1.23122E-09
b	[m ³ /kg]	-6.37801E-04	k	[-]	5.475
R	[bar m ³ /(kgK)]	1.14546E-03			

with $z = \nu - b$. The equation for specific heat capacity under ideal gas conditions (3) and the thermal equation of state (4) form the basis of the specific enthalpy and entropy calculation.

the equation for the specific enthalpy and entropy is transformed into

$$h = h_0 + (p\nu - RT) + D_1T + D_2 \frac{T^2}{2} + D_3 \frac{T^3}{3} + D_4 \ln T + \frac{E_1}{z} + \frac{E_2}{2z^2} + \frac{E_3}{3z^3} + \frac{E_4}{4z^4} + e^{-kT_R} \cdot (1 + k \cdot T_R) \cdot \left(\frac{G_1}{z} + \frac{G_2}{2z^2} + \frac{G_4}{4z^4} \right) \quad (5)$$

and

$$s = s_0 + R \ln \left(\frac{zp_l}{RT} \right) + D_1 \cdot \ln T + D_2T + D_3 \frac{T^2}{2} - \frac{D_4}{T} - \left(\frac{F_1}{z} + \frac{F_2}{2z^2} + \frac{F_4}{4z^4} \right) + \frac{k}{T_c} e^{-kT_R} \left(\frac{G_1}{z} + \frac{G_2}{2z^2} + \frac{G_4}{4z^4} \right) \quad (6)$$

with $z = \nu - b$ and $p_f = 1,013 \text{ bar}$.

The Clausius - Clapeyron equation was used to generate thermodynamic data in the wet vapour range.

$$\frac{dp}{dT} = \frac{1}{T} \cdot \frac{h''-h'}{v''-v'} \quad (7)$$

Rearranging equation (7) gives

$$h' = h'' - \frac{dp}{dT} \cdot T \cdot (v''-v') \quad (8)$$

The intergration constants h_0 und s_0 are found by letting

$$h'_{(t=0^\circ\text{C})} = 200.0 \text{ kJ/kg}$$

$$s'_{(t=0^\circ\text{C})} = 1.000 \text{ kJ/(kg K)}$$

to be

$$h_0 = 363.80 \text{ kJ/kg}$$

$$s_0 = -2.5079 \text{ kJ/(kg K)}$$

If neither the kinetic nor the potential energies are taken into account, the specific exergy may be found by the following equation:

$$e = h - h_u - T_u (s - s_u) \quad (9)$$

where the subscript u indicates ambient conditions.

The saturation pressure of the substance at $T_u = 290 \text{ K}$ serves as the reference pressure.

Applying the preconditions mentioned above, the constants h_u and s_u are found to be as follows:

$$h_u = 226.04 \text{ kJ/kg}$$

$$s_u = 1.0908 \text{ kJ/(kg K)},$$

for which specific exergy is set to $e = 0$ according to existing agreements.

3.3 Transport Properties

3.3.1 Dynamic Viscosity of Saturated Liquid

The viscosity of the saturated liquid of Solkane®410 was measured within the temperature range of -50 to 60 °C. The following regression equation is valid for the liquid phase:

$$\ln\left(\frac{\eta'}{10^{-3}}\right) = H_0 + H_1 t + H_2 t^2 + H_3 t^3 \quad (10)$$

with t in °C and η' in 10^{-3} Pa s. The coefficients are:

$$\begin{aligned} H_0 &= -1.78743 & [\text{Pa s}] & & H_2 &= -2.0903e^{-5} & [\text{Pa s/K}^2] \\ H_1 &= -0.012082 & [\text{Pa s/K}] & & H_3 &= -2.3930e^{-7} & [\text{Pa s/K}^3] \end{aligned}$$

Saturated liquid viscosity η' in 10^{-3} Pa s

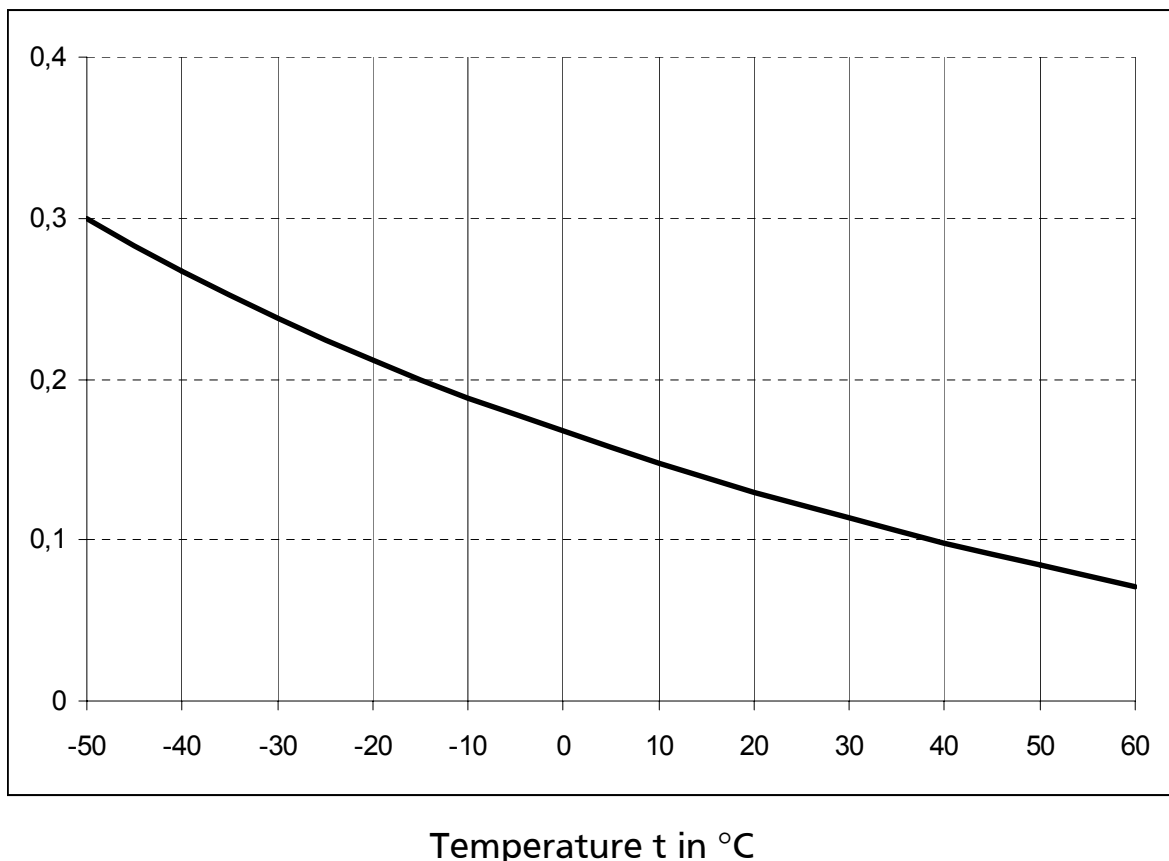


Figure 1: Dynamic viscosity of the saturated liquid

3.3.2 Dynamic Viscosity of Saturated and Superheated Vapour

The viscosity of the saturated and superheated vapour of Solkane®410 was measured in a temperature range of -50 to 50°C. The data can be represented by the following equations

$$\eta = \eta_0 + \Delta\eta \quad (11)$$

with

$$\eta_0 = 2.6696 \times 10^{-2} \times \frac{(MT)^{\frac{1}{2}}}{\sigma^2 \Omega_\eta T^*}, \quad T^* = \frac{kT}{\varepsilon} \text{ and}$$

$$\Omega(T^*) = \exp[0.45667 - 0.53955(\ln T^*) + 0.187265(\ln T^*)^2 - 0.03629(\ln T^*)^3 + 0.00241(\ln T^*)^4] \quad (12 \text{ a-c})$$

$$\Delta\eta = T_R^{2.2} \left[\ln(1.65 + \rho_{R0}^{0.8}) \right]^{1.6} \left[e^{\left(1 - \frac{0.78}{T_c}\right) \rho_{r0}} - 1 \right] (F \cdot z_c \cdot \zeta)^{-1}$$

$$z_c = \frac{p_c V_c}{RT_c} \quad \text{and} \quad \rho_{R0} = \frac{\rho - \rho_0}{\rho_c} \quad \text{and} \quad F = 1 \text{ for Solkane®410 as a light polar agent.}$$

(12 d-f)

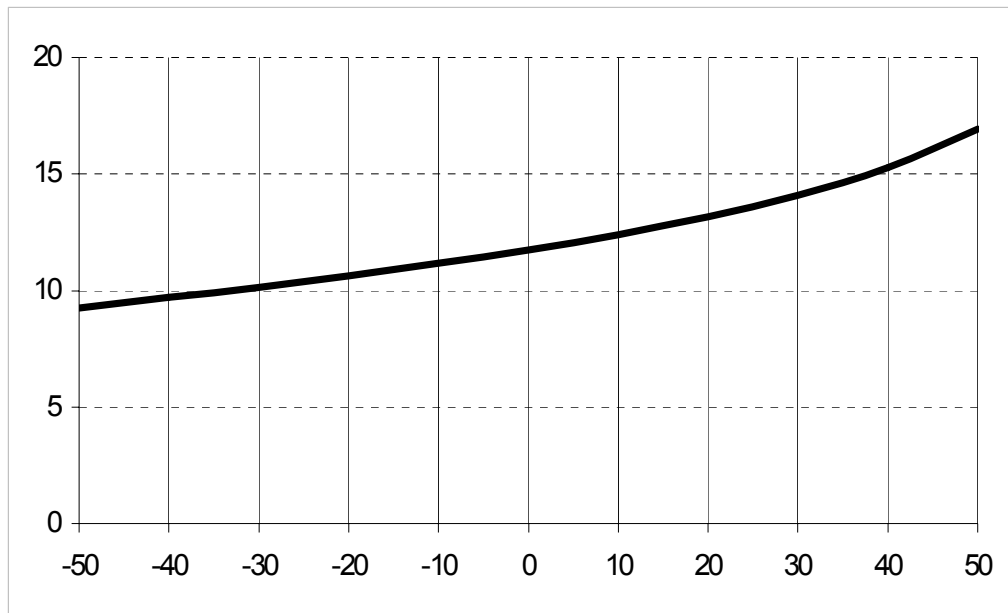
In equation (12) the constants are as follows .

R the universal gas constant	= 8314	[J kmol ⁻¹ K ⁻¹]
ρ_c the critical density	= 487.37	[kg/m ³]
ρ_0 the density at 1.013bar and temperature as defined by T		[kg/m ³]
T_c the critical temperature	= 344.95	[K]

The constants of equation (11) were determined to be

$$\begin{aligned} \zeta &= 40990.75 \text{ [1/(Pa s)]} \\ \sigma &= 0.4324 \text{ [nm]} \\ \varepsilon/k &= 317.47 \text{ [K]} \end{aligned}$$

Saturated vapor viscosity η'' in 10^{-6} Pa s



Temperature t in $^{\circ}\text{C}$

Figure 2: Dynamic viscosity of saturated vapour

3.3.3 Thermal Conductivity of Saturated Liquid

The thermal conductivity of saturated liquid can be expressed with the regression equation

$$\lambda' = J_0 + J_1 t \quad (13)$$

where t is in °C and λ' in $10^{-3}\text{W}/(\text{mK})$. The coefficients of the equation are:

$$J_0 = 99.926 \quad [10^{-3}\text{W}/(\text{mK})] \quad J_1 = -0.5071 \quad [10^{-3}\text{W}/(\text{mK}^2)]$$

Thermal conductivity of saturated liquid λ' in $10^{-3}\text{ W}/(\text{m K})$

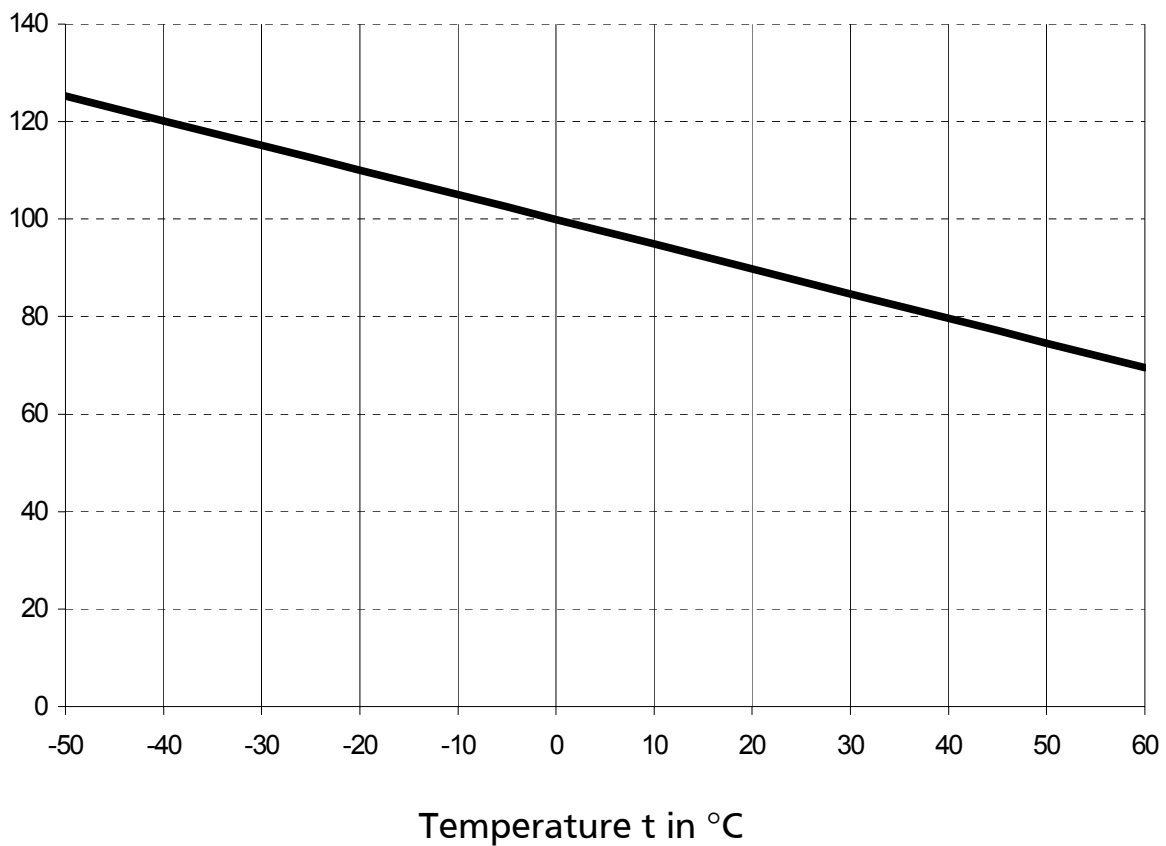


Figure 3: Thermal conductivity of saturated liquid

3.3.4 Thermal Conductivity of Saturated Vapour

The thermal conductivity of saturated vapour can be expressed using the regression equation

$$\lambda'' = K_0 + K_1 t + K_2 t^2 + K_3 t^3 + K_4 t^4 \quad (14)$$

where t is in °C and λ'' in 10^{-3} W/(m K). The coefficients of the equation are as follows:

$K_0 =$	13.061	$[10^{-3}\text{W}/(\text{mK})]$	$K_3 =$	3.3487e^{-6}	$[10^{-3}\text{W}/(\text{m K}^4)]$
$K_1 =$	0.10279	$[10^{-3}\text{W}/(\text{mK}^2)]$	$K_4 =$	-2.5798e^{-8}	$[10^{-3}\text{W}/(\text{m K}^5)]$
$K_2 =$	1.3743e^{-3}	$[10^{-3}\text{W}/(\text{mK}^3)]$			

Thermal conductivity of saturated vapour λ'' in 10^{-3} W/(mK)

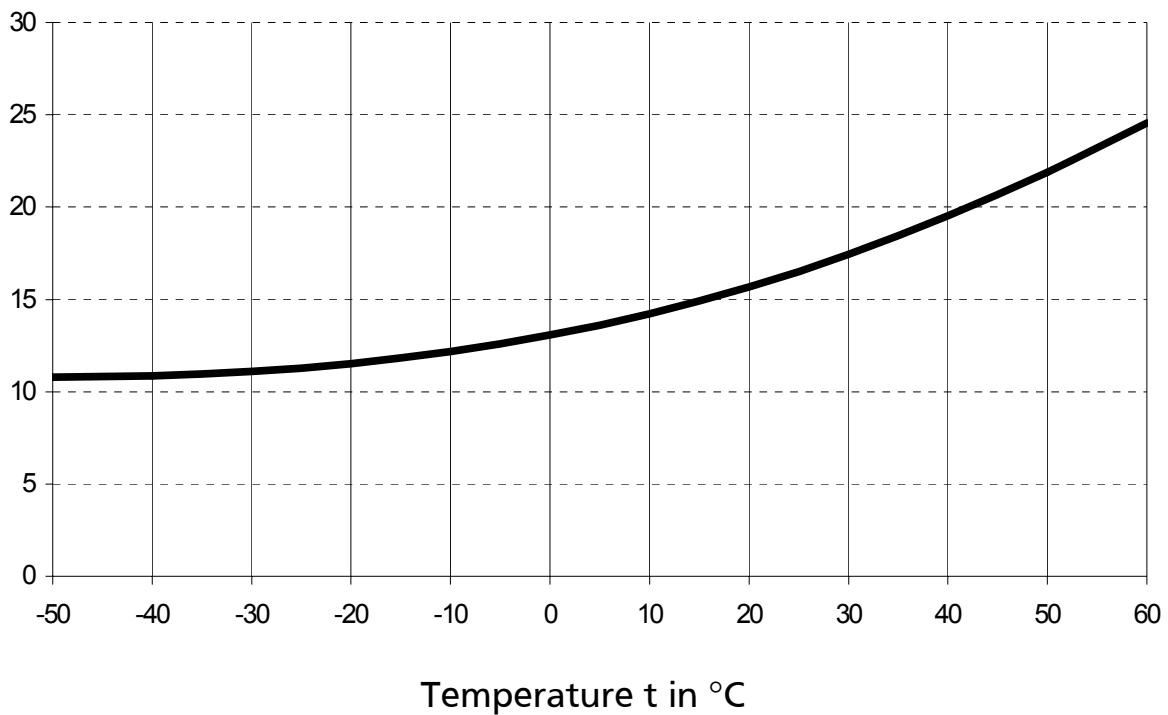


Figure 4: Thermal conductivity of saturated vapour

3.3.5 Surface Tension

The surface tension of the liquid can be expressed using the regression equation

$$\sigma = L_0 + L_1 t + L_2 t^2 + L_3 t^3 \quad (15)$$

where t is in °C and σ in 10^{-3} N/m. The coefficients of the equation are:

$$\begin{array}{llll} L_0 = 8.7963 & [10^{-3}\text{N/m}] & L_2 = 2.1740\text{e}^{-4} & [10^{-3}\text{N}/(\text{mK}^2)] \\ L_1 = -0.15227 & [10^{-3}\text{N}/(\text{mK})] & L_3 = 2.1147\text{e}^{-6} & [10^{-3}\text{N}/(\text{mK}^3)] \end{array}$$

Surface tension σ in 10^{-3} N/m

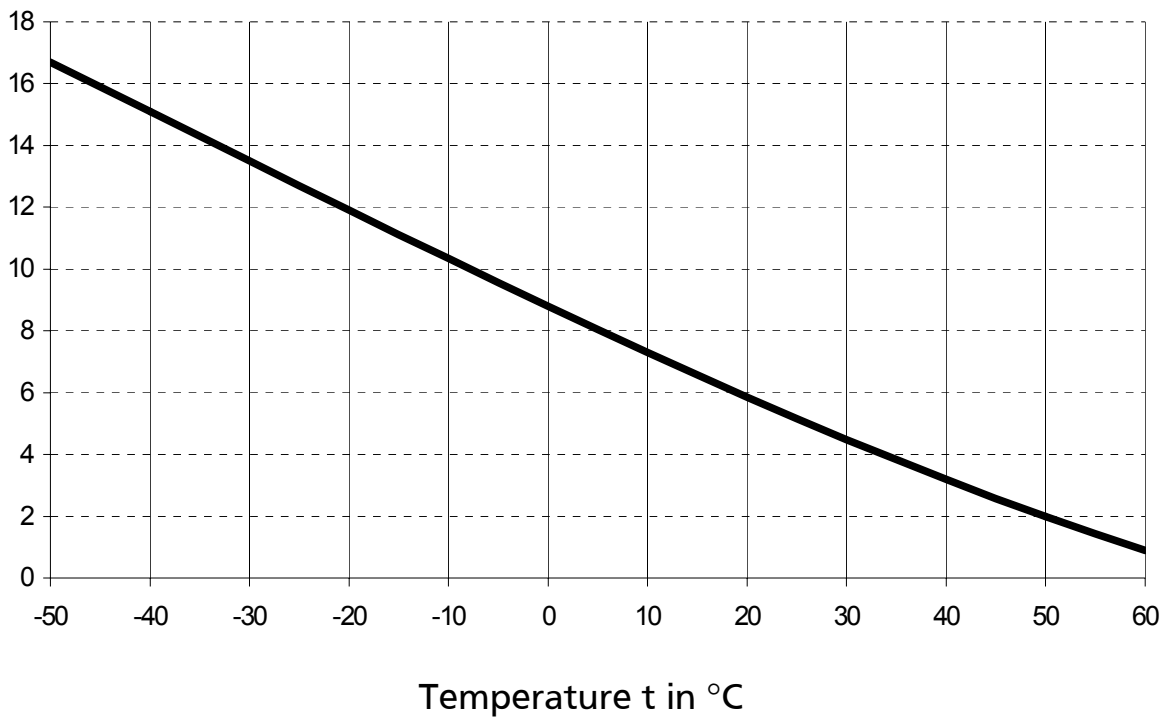


Figure 5: Surface tension

3.3.6 Specific Heat Capacity of Saturated Liquid

The specific heat capacity of saturated liquid can be expressed using the equation

$$c'_p = M_0 + M_1(1 - T_R)^{1/9} + M_2(1 - T_R)^{2/9} + M_3(1 - T_R)^{3/9} + M_4(1 - T_R)^{6/9} \quad (16)$$

where $T_R = \frac{T}{T_c}$, c'_p is in kJ/(kg K) and T is in K. The coefficients of the equation are as follows:

$$\begin{aligned} M_0 &= 237.48544 \quad [\text{kJ}/(\text{kgK})] & M_3 &= -734.81854 \quad [\text{kJ}/(\text{kgK})] \\ M_1 &= -974.66894 \quad [\text{kJ}/(\text{kgK})] & M_4 &= 60.886696 \quad [\text{kJ}/(\text{kgK})] \\ M_2 &= 1412.81 \quad [\text{kJ}/(\text{kgK})] \end{aligned}$$

Specific heat capacity of saturated liquid c_p' in kJ/(kgK)

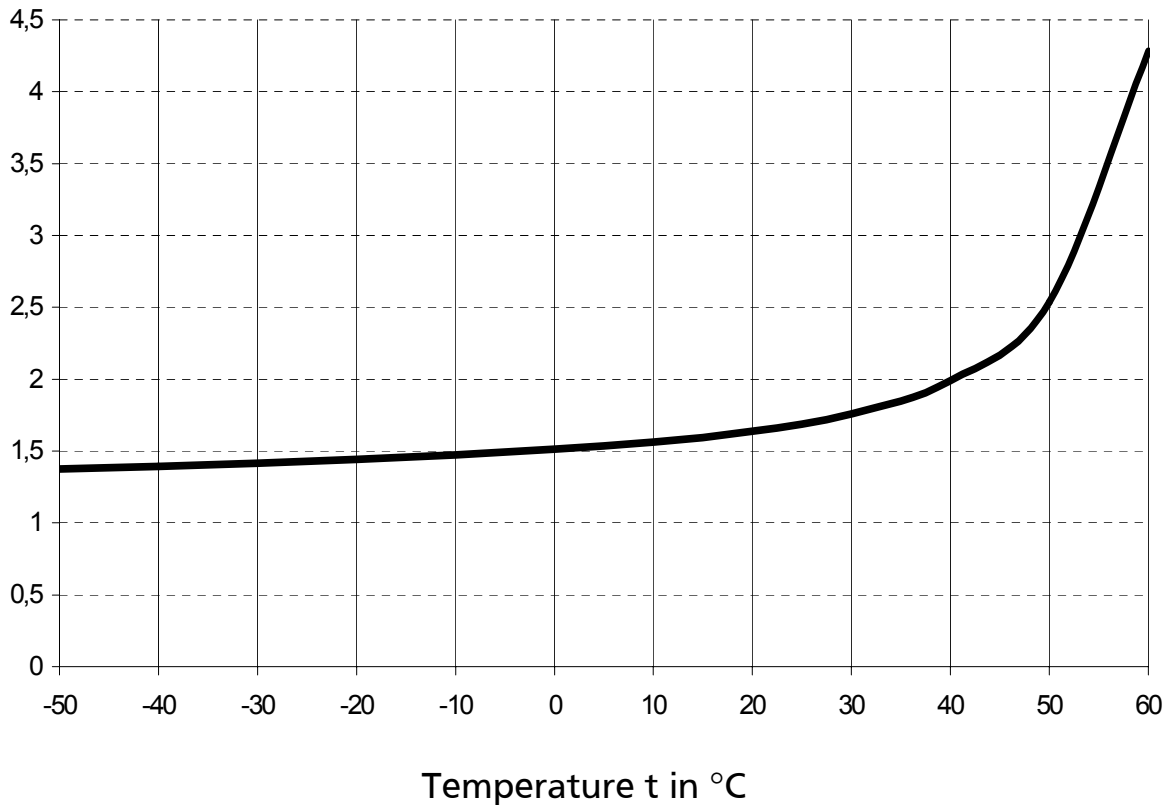


Figure 6: Specific heat capacity of saturated liquid

4 Compatibility of Materials

4.1 Elastomeres

The compatibility of the elastomeres that are normally used in refrigeration systems with Solkane®410 is generally good. Cold extraction tests that were carried out on CR (chlorbutadiene rubber or Neoprene®), NBR (acrylonitrilebutadienerubber) and HNBR (hydrated acrylnitrilbutadiene rubber) showed only slight swelling and yielded negligible amounts of extract. Fluorinated rubbers (FKM and FPM) are not recommended because of their considerable swelling and blistering when used with Solkane®410 or with other HFC refrigerants. Ethylenepropylenediene rubber is only to be recommended where the presence of mineral oil in the refrigeration cycle can be excluded.

The effect of the lubricant that is used must not be ignored. Recommendations made by the lubricant and compressor manufacturers must be followed.

4.2 Thermoplastics

Experience with CFC and HCFC has shown that only a limited number of plastics are resistant to fluorinated refrigerants. Polytetrafluoroethylene, polyacetale and polyamide might be taken into account for the use with Solkane®410. It is again vital to take the effect of the lubricant into account.

4.3 Metals

Solkane®410 is generally used in conjunction with lubricants (Ester oils, PAG-oils) in refrigeration technology. In combination both materials are compatible with the metals and alloys usually found in machines and apparatus. Only zinc, magnesium, lead and aluminium alloys with more than 2% magnesium by mass should be avoided. The water content of refrigeration oil depending on oil type should especially be taken into account. Values of not more than 50 ppm are to be aimed at.

5 Refrigerant Oils

Like all fluorinated hydrocarbons, Solkane[®]410 is immiscible with mineral oils. Ester oils (POE) are normally used as lubricants. The solubility of these oils in Solkane[®]410 is a function of temperature and composition. The following diagrams show the solubility properties of various lubricants with Solkane[®]410. Highly viscous lubricants tend to give large miscibility gaps.

The precise miscibility gaps of the individual oils can be obtained from the lubricant manufacturers.

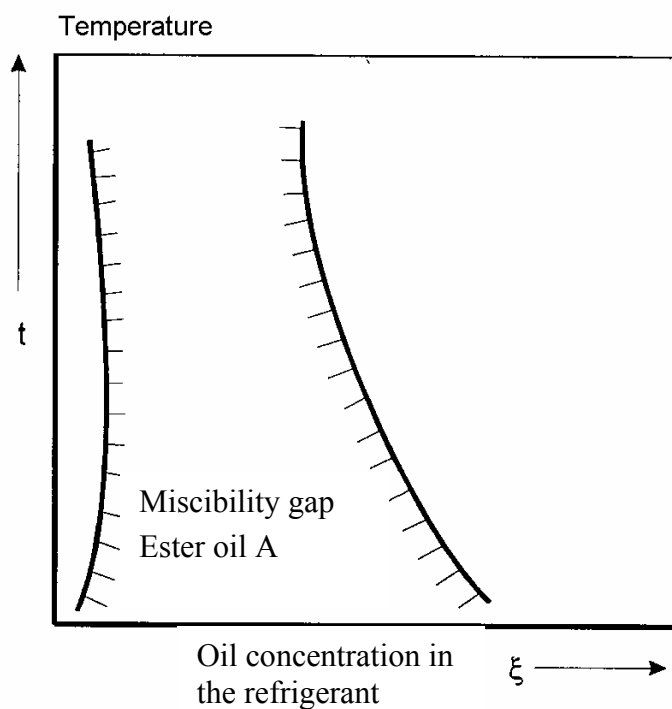


Figure 7: Miscibility behaviour of Solkane[®]410 and ester oil A

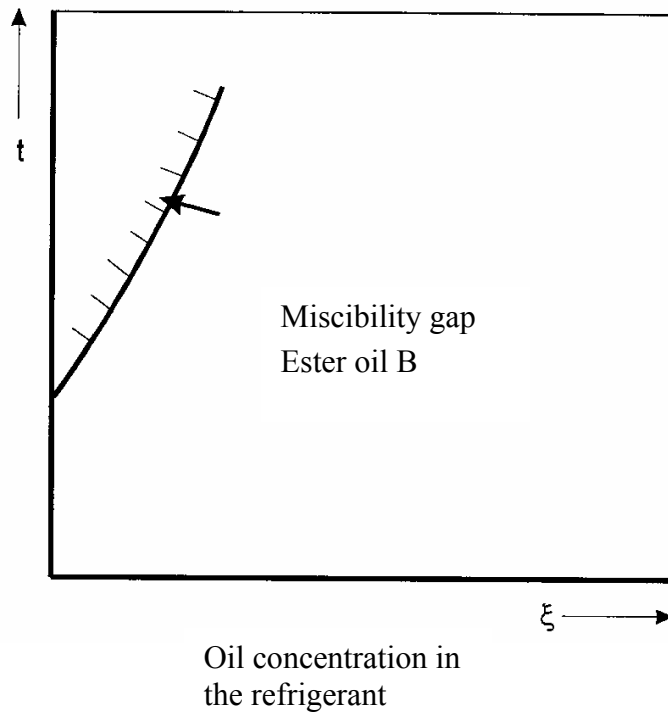


Figure 8: Miscibility behaviour of Solkane®410 and ester oil B

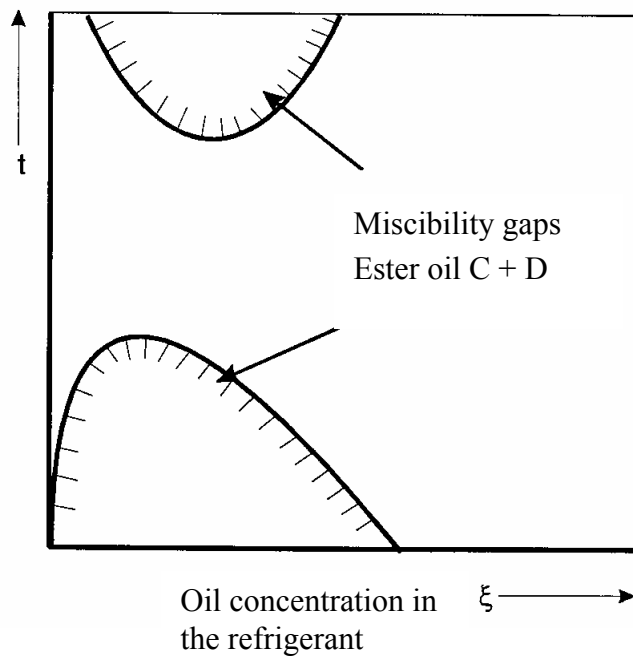


Figure 9: Miscibility behaviour of Solkane®410 and ester oil C

6 Flammability

R32 as a pure component is flammable, whereas R125 is not. According to DIN 51649 and UL 2182 Solkane®410 is not flammable.

7 Toxicity

The toxicity of R32 and R125 was extensively tested within the scope of the PAFT programme (Programme for Alternative Fluorocarbon Toxicity Testing). PAFT recommended an occupational exposure limit of 1000 ppm for both products. The toxicity of Solkane®410 can therefore be regarded as low and comparable to the toxicity of R22.

8 Vapour Table, Wet Vapour Range Solkane®410

t	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
-70	0.36	0.36	0.711	631.36	1.407	1.58	102.05	388.31	286.26	0.5924	1.9981
-69	0.38	0.38	0.712	596.08	1.404	1.68	103.44	388.89	285.45	0.5986	1.9940
-68	0.41	0.41	0.714	563.13	1.401	1.78	104.82	389.46	284.64	0.6047	1.9900
-67	0.43	0.43	0.715	532.34	1.398	1.88	106.19	390.03	283.84	0.6109	1.9860
-66	0.46	0.46	0.717	503.54	1.395	1.99	107.56	390.60	283.04	0.6171	1.9821
-65	0.49	0.49	0.718	476.59	1.392	2.10	108.92	391.17	282.24	0.6232	1.9783
-64	0.52	0.52	0.720	451.35	1.389	2.22	110.28	391.73	281.45	0.6294	1.9745
-63	0.55	0.55	0.722	427.69	1.386	2.34	111.63	392.29	280.66	0.6356	1.9708
-62	0.58	0.58	0.723	405.50	1.383	2.47	112.98	392.85	279.87	0.6417	1.9671
-61	0.61	0.61	0.725	384.69	1.380	2.60	114.33	393.41	279.08	0.6479	1.9635
-60	0.65	0.65	0.726	365.15	1.377	2.74	115.67	393.96	278.29	0.6540	1.9599
-59	0.69	0.68	0.728	346.79	1.374	2.88	117.01	394.52	277.50	0.6601	1.9564
-58	0.72	0.72	0.729	329.53	1.371	3.03	118.35	395.07	276.71	0.6663	1.9529
-57	0.76	0.76	0.731	313.29	1.368	3.19	119.69	395.61	275.92	0.6724	1.9495
-56	0.81	0.80	0.733	298.01	1.365	3.36	121.03	396.16	275.13	0.6785	1.9461
-55	0.85	0.85	0.734	283.61	1.362	3.53	122.37	396.70	274.33	0.6846	1.9428
-54	0.90	0.89	0.736	270.05	1.359	3.70	123.70	397.24	273.54	0.6907	1.9395
-53	0.94	0.94	0.738	257.26	1.355	3.89	125.04	397.78	272.74	0.6968	1.9363
-52	0.99	0.99	0.739	245.19	1.352	4.08	126.38	398.31	271.93	0.7029	1.9331
-51	1.04	1.04	0.741	233.80	1.349	4.28	127.72	398.84	271.12	0.7089	1.9300
-50	1.10	1.10	0.743	223.04	1.346	4.48	129.06	399.37	270.31	0.7150	1.9268
-49	1.15	1.15	0.745	212.88	1.343	4.70	130.40	399.90	269.50	0.7210	1.9238
-48	1.21	1.21	0.746	203.27	1.340	4.92	131.74	400.42	268.68	0.7271	1.9207
-47	1.27	1.27	0.748	194.18	1.337	5.15	133.09	400.94	267.85	0.7331	1.9178
-46	1.33	1.33	0.750	185.57	1.333	5.39	134.44	401.46	267.02	0.7391	1.9148
-45	1.40	1.40	0.752	177.42	1.330	5.64	135.79	401.97	266.18	0.7451	1.9119
-44	1.47	1.46	0.754	169.70	1.327	5.89	137.14	402.48	265.34	0.7511	1.9090
-43	1.54	1.53	0.755	162.38	1.324	6.16	138.49	402.99	264.49	0.7570	1.9062
-42	1.61	1.61	0.757	155.44	1.321	6.43	139.85	403.49	263.64	0.7630	1.9034
-41	1.68	1.68	0.759	148.86	1.317	6.72	141.21	403.99	262.78	0.7689	1.9006
-40	1.76	1.76	0.761	142.61	1.314	7.01	142.58	404.49	261.91	0.7749	1.8979
-39	1.84	1.84	0.763	136.67	1.311	7.32	143.94	404.98	261.04	0.7808	1.8952
-38	1.93	1.92	0.765	131.03	1.308	7.63	145.31	405.47	260.16	0.7867	1.8925
-37	2.01	2.01	0.767	125.67	1.304	7.96	146.69	405.96	259.27	0.7925	1.8898
-36	2.10	2.10	0.769	120.57	1.301	8.29	148.07	406.44	258.37	0.7984	1.8872
-35	2.20	2.19	0.771	115.72	1.298	8.64	149.45	406.92	257.47	0.8043	1.8846
-34	2.29	2.29	0.773	111.10	1.294	9.00	150.83	407.39	256.56	0.8101	1.8821
-33	2.39	2.39	0.775	106.71	1.291	9.37	152.22	407.86	255.64	0.8159	1.8796
-32	2.49	2.49	0.777	102.52	1.288	9.75	153.61	408.33	254.72	0.8217	1.8771
-31	2.60	2.59	0.779	98.53	1.284	10.15	155.01	408.79	253.79	0.8275	1.8746

Vapour Table, Wet Vapour Range Solkane®410

t	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
-30	2.71	2.70	0.781	94.72	1.281	10.56	156.41	409.25	252.85	0.8333	1.8721
-29	2.82	2.81	0.783	91.09	1.278	10.98	157.81	409.71	251.90	0.8391	1.8697
-28	2.94	2.93	0.785	87.63	1.274	11.41	159.22	410.16	250.94	0.8448	1.8673
-27	3.06	3.05	0.787	84.32	1.271	11.86	160.63	410.61	249.98	0.8505	1.8650
-26	3.18	3.17	0.789	81.16	1.267	12.32	162.04	411.05	249.01	0.8562	1.8626
-25	3.31	3.30	0.791	78.15	1.264	12.80	163.46	411.49	248.03	0.8619	1.8603
-24	3.44	3.43	0.793	75.27	1.260	13.29	164.88	411.92	247.04	0.8676	1.8580
-23	3.58	3.57	0.796	72.51	1.257	13.79	166.31	412.35	246.04	0.8733	1.8557
-22	3.72	3.71	0.798	69.87	1.253	14.31	167.74	412.78	245.04	0.8789	1.8535
-21	3.86	3.85	0.800	67.35	1.250	14.85	169.18	413.20	244.03	0.8846	1.8512
-20	4.01	4.00	0.802	64.94	1.246	15.40	170.61	413.62	243.00	0.8902	1.8490
-19	4.16	4.15	0.805	62.63	1.243	15.97	172.06	414.03	241.97	0.8958	1.8468
-18	4.32	4.31	0.807	60.42	1.239	16.55	173.50	414.44	240.94	0.9014	1.8446
-17	4.48	4.47	0.809	58.30	1.235	17.15	174.95	414.84	239.89	0.9070	1.8425
-16	4.65	4.63	0.812	56.26	1.232	17.77	176.40	415.24	238.83	0.9125	1.8403
-15	4.82	4.80	0.814	54.32	1.228	18.41	177.86	415.63	237.77	0.9181	1.8382
-14	4.99	4.98	0.817	52.45	1.224	19.07	179.32	416.01	236.70	0.9236	1.8361
-13	5.17	5.16	0.819	50.65	1.221	19.74	180.78	416.40	235.61	0.9292	1.8340
-12	5.36	5.34	0.822	48.93	1.217	20.44	182.25	416.77	234.52	0.9347	1.8319
-11	5.55	5.53	0.824	47.28	1.213	21.15	183.72	417.14	233.42	0.9402	1.8299
-10	5.74	5.72	0.827	45.70	1.210	21.88	185.20	417.51	232.31	0.9457	1.8278
-9	5.94	5.92	0.829	44.17	1.206	22.64	186.67	417.87	231.20	0.9511	1.8258
-8	6.15	6.13	0.832	42.71	1.202	23.42	188.15	418.22	230.07	0.9566	1.8238
-7	6.36	6.34	0.835	41.30	1.198	24.21	189.64	418.57	228.93	0.9621	1.8218
-6	6.57	6.55	0.837	39.95	1.194	25.03	191.13	418.92	227.79	0.9675	1.8198
-5	6.80	6.78	0.840	38.64	1.191	25.88	192.62	419.25	226.63	0.9730	1.8178
-4	7.02	7.00	0.843	37.39	1.187	26.74	194.12	419.59	225.47	0.9784	1.8158
-3	7.26	7.23	0.845	36.19	1.183	27.63	195.62	419.91	224.29	0.9838	1.8138
-2	7.50	7.47	0.848	35.03	1.179	28.55	197.12	420.23	223.11	0.9892	1.8119
-1	7.74	7.72	0.851	33.91	1.175	29.49	198.62	420.54	221.92	0.9946	1.8099
0	7.99	7.97	0.854	32.83	1.171	30.46	200.00	420.85	220.85	1.0000	1.8080
1	8.25	8.22	0.857	31.80	1.167	31.45	201.65	421.15	219.50	1.0054	1.8061
2	8.51	8.49	0.860	30.80	1.163	32.47	203.17	421.44	218.27	1.0108	1.8041
3	8.78	8.75	0.863	29.83	1.159	33.52	204.69	421.72	217.03	1.0161	1.8022
4	9.06	9.03	0.866	28.90	1.155	34.60	206.21	422.00	215.79	1.0215	1.8003
5	9.34	9.31	0.869	28.01	1.151	35.70	207.74	422.27	214.53	1.0269	1.7984
6	9.63	9.60	0.872	27.14	1.146	36.84	209.28	422.53	213.26	1.0322	1.7965
7	9.92	9.89	0.875	26.31	1.142	38.01	210.81	422.79	211.98	1.0376	1.7946
8	10.23	10.20	0.879	25.50	1.138	39.21	212.36	423.04	210.68	1.0430	1.7927
9	10.54	10.50	0.882	24.73	1.134	40.44	213.90	423.28	209.37	1.0483	1.7908

Vapour Table, Wet Vapour Range Solkane®410

t	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
10	10.85	10.82	0.885	23.97	1.130	41.71	215.45	423.51	208.05	1.0537	1.7889
11	11.18	11.14	0.889	23.25	1.125	43.01	217.01	423.73	206.72	1.0590	1.7870
12	11.51	11.47	0.892	22.55	1.121	44.35	218.57	423.95	205.38	1.0644	1.7851
13	11.85	11.81	0.896	21.87	1.116	45.73	220.14	424.15	204.02	1.0698	1.7832
14	12.19	12.15	0.899	21.21	1.112	47.14	221.71	424.35	202.64	1.0751	1.7813
15	12.54	12.51	0.903	20.58	1.108	48.59	223.29	424.54	201.25	1.0805	1.7794
16	12.90	12.87	0.907	19.97	1.103	50.09	224.87	424.71	199.85	1.0859	1.7775
17	13.27	13.23	0.910	19.37	1.099	51.62	226.46	424.88	198.43	1.0912	1.7756
18	13.65	13.61	0.914	18.80	1.094	53.20	228.05	425.04	196.99	1.0966	1.7736
19	14.03	13.99	0.918	18.24	1.089	54.82	229.65	425.19	195.53	1.1020	1.7717
20	14.43	14.38	0.922	17.70	1.085	56.49	231.26	425.32	194.06	1.1074	1.7698
21	14.83	14.78	0.926	17.18	1.080	58.20	232.88	425.45	192.57	1.1128	1.7678
22	15.24	15.19	0.930	16.68	1.075	59.96	234.50	425.57	191.06	1.1183	1.7659
23	15.65	15.61	0.934	16.19	1.070	61.78	236.13	425.67	189.54	1.1237	1.7639
24	16.08	16.03	0.939	15.71	1.066	63.64	237.77	425.76	187.99	1.1291	1.7619
25	16.52	16.47	0.943	15.25	1.061	65.56	239.42	425.84	186.42	1.1346	1.7599
26	16.96	16.91	0.947	14.81	1.056	67.54	241.08	425.91	184.82	1.1401	1.7579
27	17.41	17.36	0.952	14.37	1.051	69.57	242.75	425.96	183.21	1.1455	1.7559
28	17.87	17.82	0.956	13.95	1.046	71.67	244.43	426.00	181.57	1.1510	1.7539
29	18.34	18.29	0.961	13.55	1.040	73.83	246.11	426.02	179.91	1.1566	1.7518
30	18.82	18.77	0.966	13.15	1.035	76.05	247.81	426.03	178.22	1.1621	1.7497
31	19.31	19.26	0.971	12.77	1.030	78.34	249.53	426.03	176.50	1.1677	1.7476
32	19.81	19.76	0.976	12.39	1.025	80.70	251.25	426.01	174.76	1.1733	1.7455
33	20.32	20.26	0.981	12.03	1.019	83.13	252.99	425.97	172.99	1.1789	1.7434
34	20.84	20.78	0.987	11.68	1.014	85.64	254.73	425.92	171.18	1.1845	1.7412
35	21.37	21.31	0.992	11.33	1.008	88.23	256.50	425.85	169.35	1.1901	1.7390
36	21.91	21.85	0.998	11.00	1.002	90.90	258.28	425.76	167.48	1.1958	1.7367
37	22.46	22.40	1.003	10.68	0.997	93.65	260.07	425.65	165.58	1.2015	1.7345
38	23.02	22.95	1.009	10.36	0.991	96.50	261.88	425.52	163.64	1.2073	1.7322
39	23.59	23.52	1.015	10.06	0.985	99.45	263.71	425.37	161.66	1.2130	1.7298
40	24.17	24.10	1.021	9.76	0.979	102.49	265.56	425.20	159.64	1.2188	1.7274
41	24.76	24.69	1.028	9.47	0.973	105.64	267.42	425.00	157.59	1.2247	1.7250
42	25.37	25.30	1.034	9.18	0.967	108.90	269.30	424.79	155.48	1.2306	1.7225
43	25.98	25.91	1.041	8.91	0.960	112.28	271.21	424.54	153.34	1.2365	1.7200
44	26.61	26.54	1.048	8.64	0.954	115.78	273.13	424.27	151.14	1.2424	1.7174
45	27.24	27.17	1.056	8.37	0.947	119.41	275.08	423.98	148.90	1.2484	1.7148
46	27.89	27.82	1.063	8.12	0.941	123.17	277.05	423.65	146.60	1.2544	1.7121
47	28.55	28.48	1.071	7.87	0.934	127.09	279.04	423.29	144.25	1.2605	1.7093
48	29.23	29.15	1.079	7.62	0.927	131.16	281.06	422.90	141.84	1.2666	1.7065
49	29.91	29.84	1.088	7.39	0.919	135.39	283.11	422.47	139.37	1.2727	1.7035

Vapour Table, Wet Vapour Range Solkane®410

t	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
50	30.61	30.53	1.096	7.15	0.912	139.81	285.18	422.01	136.83	1.2789	1.7005
51	31.32	31.24	1.106	6.92	0.905	144.41	287.28	421.51	134.23	1.2852	1.6974
52	32.04	31.97	1.115	6.70	0.897	149.23	289.41	420.96	131.55	1.2915	1.6942
53	32.78	32.70	1.125	6.48	0.889	154.26	291.57	420.37	128.79	1.2978	1.6909
54	33.53	33.45	1.136	6.27	0.880	159.54	293.77	419.72	125.96	1.3042	1.6875
55	34.29	34.22	1.147	6.06	0.872	165.08	296.00	419.03	123.03	1.3107	1.6839
56	35.07	35.00	1.159	5.85	0.863	170.91	298.26	418.27	120.01	1.3172	1.6802
57	35.86	35.79	1.171	5.65	0.854	177.06	300.56	417.45	116.89	1.3238	1.6763
58	36.67	36.59	1.185	5.45	0.844	183.56	302.89	416.55	113.66	1.3304	1.6723
59	37.49	37.42	1.199	5.25	0.834	190.46	305.27	415.58	110.31	1.3371	1.6680
60	38.32	38.25	1.214	5.06	0.824	197.81	307.68	414.51	106.83	1.3439	1.6635
61	39.18	39.11	1.231	4.86	0.813	205.68	310.14	413.35	103.21	1.3507	1.6588
62	40.04	39.97	1.249	4.67	0.801	214.13	312.64	412.06	99.42	1.3576	1.6537
63	40.93	40.86	1.269	4.48	0.788	223.29	315.18	410.63	95.45	1.3645	1.6482
64	41.83	41.76	1.291	4.29	0.774	233.28	317.77	409.04	91.27	1.3716	1.6423
65	42.74	42.68	1.317	4.09	0.759	244.30	320.41	407.24	86.83	1.3787	1.6358
66	43.68	43.62	1.347	3.90	0.743	256.65	323.10	405.19	82.09	1.3858	1.6287

9 Vapour Table, Superheated Range Solkane® 410

0.36 bar -70.00 °C					0.52 bar -64.00 °C					0.72 bar -58.00 °C					0.99 bar -52.00 °C				
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	
°C	dm ³ /kg	kJ/kg	kJ/kgK																
-70	631.36	388.31	1.9981																
-65	648.17	391.80	2.0150																
-60	664.89	395.31	2.0317																
-55	681.54	398.84	2.0480																
-50	698.11	402.40	2.0642																
-45	714.62	405.98	2.0801																
-40	731.07	409.60	2.0957																
-35	747.47	413.24	2.1112																
-30	763.83	416.91	2.1264																
-25	780.14	420.62	2.1415																
-20	796.42	424.35	2.1564																
-15	812.67	428.12	2.1711																
-10	828.89	431.91	2.1857																
-5	845.08	435.75	2.2001																
0	861.24	439.61	2.2144																
5	877.38	443.51	2.2286																
10	893.51	447.45	2.2426																
15	909.61	451.42	2.2565																
<hr/>					<hr/>					<hr/>					<hr/>				
0.41 bar -68.00 °C					0.58 bar -62.00 °C					0.81 bar -56.00 °C					1.10 bar -50.00 °C				
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	
°C	dm ³ /kg	kJ/kg	kJ/kgK																
-68	563.13	389.46	1.9900																
-65	572.11	391.57	2.0002																
-60	587.01	395.09	2.0169																
-55	601.83	398.64	2.0333																
-50	616.58	402.21	2.0495																
-45	631.27	405.81	2.0655																
-40	645.89	409.43	2.0812																
-35	660.47	413.09	2.0967																
-30	675.00	416.77	2.1120																
-25	689.49	420.48	2.1271																
-20	703.95	424.22	2.1420																
-15	718.37	428.00	2.1568																
-10	732.76	431.80	2.1714																
-5	747.12	435.64	2.1859																
0	761.46	439.51	2.2002																
5	775.78	443.42	2.2143																
10	790.08	447.36	2.2284																
15	804.36	451.33	2.2423																
<hr/>					<hr/>					<hr/>					<hr/>				
0.46 bar -66.00 °C					0.65 bar -60.00 °C					0.89 bar -54.00 °C					1.21 bar -48.00 °C				
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	
°C	dm ³ /kg	kJ/kg	kJ/kgK																
-66	503.54	390.60	1.9821																
-65	506.21	391.31	1.9855																
-60	519.54	394.85	2.0024																
-55	532.78	398.41	2.0189																
-50	545.95	402.00	2.0351																
-45	559.05	405.61	2.0512																
-40	572.10	409.25	2.0669																
-35	585.10	412.92	2.0825																
-30	598.05	416.61	2.0978																
-25	610.96	420.33	2.1130																
-20	623.83	424.08	2.1279																
-15	636.67	427.86	2.1427																
-10	649.48	431.68	2.1574																
-5	662.26	435.52	2.1718																
0	675.02	439.40	2.1862																
5	687.76	443.31	2.2004																
10	700.47	447.26	2.2144																
15	713.17	451.24	2.2284																
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0.52 bar -64.00 °C					0.72 bar -58.00 °C					1.01 bar -50.00 °C					1.36 bar -48.00 °C				
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	
°C	dm ³ /kg	kJ/kg	kJ/kgK																
-64	451.35	391.73	1.9745																
-60	460.90	394.58	1.9880																
-55	472.77	398.17	2.0046																
-50	484.57	401.77	2.0210																
-45	496.31	405.40	2.0371																
-40	507.98	409.05	2.0529																
-35	519.61	412.73	2.0685																
-30	531.18	416.43	2.0839																
-25	542.72	420.17	2.0991																
-20	554.22	423.93	2.1141																
-15	565.69	427.72	2.1289																
-10	577.12	431.54	2.1436																
-5	588.53	435.39	2.1581																
0	599.91	439.28	2.1724																
5	611.28	443.20	2.1867																
10	622.62	447.15	2.2007																
15	633.94	451.14	2.2147																
20	645.25	455.16	2.2285																
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0.72 bar -58.00 °C					1.01 bar -50.00 °C					1.36 bar -48.00 °C									
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>		<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>						
°C	dm ³ /kg	kJ/kg	kJ/kgK																
-58	329.53	395.07	1.9529																
-55	334.75	397.26	1.9631																
-50	343.41	400.93	1.9797																
-45	351.99	404.62	1.9960																
-40	360.52	408.32	2.0121																
-35	368.99	412.05	2.0279																
-30	377.42	415.80	2.0435																
-25	385.80	419.57	2.0588																
-20	394.14	423.37	2.0740																
-15	402.45	427.19	2.0890																
-10	410.73	431.04	2.1037																
-5	418.98	434.93	2.1184																
0	427.20	438.84	2.1328																
5	435.40	442.78	2.1471																
10	443.59	446.75	2.1613																
15	451.75	450.76	2.1753																
20	459.90	454.80	2.1892																
25	468.03	458.87	2.2030																
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Vapour Table, Superheated Range Solkane®410

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 8.47 bar at 2.00°C. Rows range from t=2 to t=85.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 10.20 bar at 8.00°C. Rows range from t=8 to t=90.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 12.15 bar at 14.00°C. Rows range from t=14 to t=95.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 14.38 bar at 20.00°C. Rows range from t=20 to t=105.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 9.03 bar at 4.00°C. Rows range from t=4 to t=85.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 10.82 bar at 10.00°C. Rows range from t=10 to t=95.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 12.87 bar at 16.00°C. Rows range from t=16 to t=100.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 15.19 bar at 22.00°C. Rows range from t=22 to t=105.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 9.60 bar at 6.00°C. Rows range from t=6 to t=90.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 11.47 bar at 12.00°C. Rows range from t=12 to t=95.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 13.61 bar at 18.00°C. Rows range from t=18 to t=100.

Table with 5 columns: t (°C), v (dm³/kg), h (kJ/kg), s (kJ/kgK) for 16.03 bar at 24.00°C. Rows range from t=24 to t=105.

Vapour Table, Superheated Range Solkane®410

30.53 bar 50.00°C				35.00 bar 56.00°C				39.97 bar 62.00 °C			
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	<i>t</i>	<i>v</i>	<i>h</i>	<i>S</i>	<i>t</i>	<i>v</i>	<i>h</i>	<i>S</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK	°C	dm ³ /kg	kJ/kg	kJ/kgK	°C	dm ³ /kg	kJ/kg	kJ/kgK
50	7.15	422.01	1.7005	56	5.85	418.27	1.6802	62	4.67	412.06	1.6537
55	7.78	431.92	1.7310	60	6.39	427.91	1.7093	65	5.15	421.83	1.6827
60	8.30	440.53	1.7570	65	6.93	437.87	1.7390	70	5.73	433.98	1.7184
65	8.77	448.38	1.7804	70	7.39	446.59	1.7646	75	6.20	443.94	1.7472
70	9.19	455.71	1.8019	75	7.80	454.56	1.7877	80	6.60	452.74	1.7723
75	9.59	462.66	1.8220	80	8.17	462.02	1.8090	85	6.96	460.82	1.7950
80	9.96	469.33	1.8411	85	8.52	469.10	1.8289	90	7.29	468.39	1.8160
85	10.31	475.79	1.8592	90	8.85	475.90	1.8477	95	7.60	475.60	1.8357
90	10.65	482.07	1.8766	95	9.16	482.49	1.8657	100	7.89	482.52	1.8544
95	10.97	488.21	1.8934	100	9.46	488.89	1.8830	105	8.17	489.23	1.8723
100	11.29	494.25	1.9097	105	9.75	495.16	1.8997	110	8.44	495.75	1.8894
105	11.59	500.19	1.9255	110	10.03	501.31	1.9159	115	8.69	502.14	1.9060
110	11.88	506.06	1.9410	115	10.29	507.37	1.9316	120	8.94	508.41	1.9220
115	12.17	511.86	1.9560	120	10.56	513.35	1.9469	125	9.18	514.58	1.9376
120	12.45	517.62	1.9707	125	10.81	519.27	1.9618	130	9.41	520.68	1.9528
125	12.73	523.34	1.9852	130	11.06	525.14	1.9765	135	9.63	526.71	1.9677
130	13.00	529.02	1.9994	135	11.30	530.96	1.9909	140	9.86	532.68	1.9823
135	13.26	534.68	2.0133	140	11.54	536.75	2.0050	145	10.07	538.62	1.9965

31.97 bar 52.00 °C				36.59 bar 58.00 °C				41.76 bar 64.00 °C			
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK	°C	dm ³ /kg	kJ/kg	kJ/kgK	°C	dm ³ /kg	kJ/kg	kJ/kgK
52	6.70	420.96	1.6942	58	5.45	416.55	1.6723	64	4.29	409.04	1.6423
55	7.10	427.46	1.7141	60	5.75	422.09	1.6890	65	4.49	413.28	1.6549
60	7.65	436.88	1.7426	65	6.34	433.42	1.7227	70	5.19	428.35	1.6991
65	8.14	445.24	1.7675	70	6.83	442.90	1.7506	75	5.69	439.51	1.7314
70	8.57	452.94	1.7901	75	7.25	451.37	1.7751	80	6.11	449.02	1.7585
75	8.97	460.17	1.8111	80	7.63	459.19	1.7974	85	6.48	457.57	1.7826
80	9.34	467.07	1.8307	85	7.98	466.55	1.8181	90	6.82	465.50	1.8046
85	9.69	473.70	1.8494	90	8.31	473.57	1.8375	95	7.13	472.97	1.8250
90	10.02	480.14	1.8672	95	8.62	480.34	1.8560	100	7.42	480.12	1.8443
95	10.34	486.41	1.8844	100	8.91	486.90	1.8737	105	7.69	487.00	1.8626
100	10.65	492.56	1.9010	105	9.20	493.29	1.8908	110	7.95	493.68	1.8802
105	10.94	498.60	1.9171	110	9.47	499.56	1.9072	115	8.21	500.20	1.8971
110	11.23	504.56	1.9327	115	9.73	505.72	1.9232	120	8.45	506.58	1.9134
115	11.51	510.44	1.9480	120	9.99	511.79	1.9387	125	8.68	512.86	1.9293
120	11.79	516.26	1.9629	125	10.24	517.78	1.9539	130	8.91	519.04	1.9447
125	12.05	522.04	1.9775	130	10.48	523.72	1.9687	135	9.13	525.15	1.9598
130	12.32	527.78	1.9918	135	10.72	529.61	1.9832	140	9.35	531.20	1.9745
135	12.57	533.49	2.0059	140	10.95	535.46	1.9975	145	9.56	537.19	1.9889

33.74 bar 54.00°C				38.49 bar 60.00 °C				43.67 bar 66.00 °C			
<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>	<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK	°C	dm ³ /kg	kJ/kg	kJ/kgK	°C	dm ³ /kg	kJ/kg	kJ/kgK
54	6.27	419.72	1.6875	60	5.06	414.51	1.6635	66	3.90	405.19	1.6287
55	6.41	422.15	1.6949	65	5.75	428.21	1.7043	70	4.61	421.36	1.6761
60	7.02	432.73	1.7269	70	6.28	438.75	1.7353	75	5.19	434.40	1.7138
65	7.52	441.77	1.7538	75	6.72	447.86	1.7616	80	5.63	444.85	1.7437
70	7.97	449.92	1.7778	80	7.11	456.11	1.7852	85	6.02	454.00	1.7694
75	8.37	457.48	1.7997	85	7.46	463.80	1.8068	90	6.36	462.35	1.7925
80	8.74	464.64	1.8201	90	7.79	471.08	1.8270	95	6.67	470.15	1.8139
85	9.09	471.48	1.8393	95	8.10	478.05	1.8460	100	6.96	477.54	1.8338
90	9.42	478.09	1.8576	100	8.39	484.78	1.8642	105	7.23	484.63	1.8527
95	9.74	484.51	1.8752	105	8.67	491.32	1.8816	110	7.49	491.48	1.8707
100	10.04	490.78	1.8921	110	8.94	497.71	1.8984	115	7.74	498.14	1.8880
105	10.33	496.93	1.9085	115	9.20	503.98	1.9147	120	7.98	504.65	1.9046
110	10.61	502.98	1.9244	120	9.45	510.14	1.9304	125	8.21	511.04	1.9208
115	10.89	508.94	1.9398	125	9.69	516.22	1.9458	130	8.44	517.32	1.9364
120	11.15	514.84	1.9549	130	9.93	522.24	1.9608	135	8.65	523.51	1.9517
125	11.42	520.69	1.9697	135	10.16	528.19	1.9755	140	8.86	529.64	1.9666
130	11.67	526.49	1.9842	140	10.39	534.10	1.9899	145	9.07	535.70	1.9812
135	11.92	532.26	1.9984	145	10.61	539.97	2.0040	150	9.27	541.72	1.9955

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