

SOLKANE® - INFORMATION SERVICE

Solkane® 404A Thermodynamics

SOLVAY FLUOR

Technical Service - Refrigerants -

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1 Units and Symbols

Symbol	Unit	Meaning/Definition
A, B	[-]	Parameters of the Wagner equation
C	[-]	Parameter of the equation for density of boiling liquid
D	[kJ/(kgK)]	Parameter of the equation for specific heat capacity in an ideal gas state
E, F, G	[-]	Parameter of the Martin-Hou equation
I	[-]	Parameter of the equation for dynamic viscosity of vapour
J	[-]	Parameter for the boiling liquid enthalpy equation
K	[kJ/(kgK)]	Parameter for the boiling liquid entropy equation
L	[Pa s /K]	Parameter of the equation for dynamic viscosity of liquid
M	[W/(m K)]	parameter of the equation for thermal conductivity of the saturated liquid
N	[W/(m K)]	Parameter of the equation for thermal conductivity of the saturated vapour
O	[N/(m K)]	Parameter of the equation for surface tension
P	[kJ/(kg K)]	parameter of the equation for specific heat capacity of the saturated liquid
R	[bar m ³ /(kg K)]	Gas constant
b	[m ³ /kg]	Parameter of the Martin-Hou equation
c	[kJ/(kg K)]	Specific heat capacity
e	[kJ/kg]	Specific exergy
h	[kJ/kg]	Specific enthalpy
k	[-]	Parameter of the Martin-Hou equation
p	[bar]	Pressure
r	[kJ/kg]	Enthalpy of vaporisation
s	[kJ/(kg K)]	Specific entropy
t	[°C]	Temperature
t	[K]	Temperature
v	[m ³ /kg]	Specific volume
η	[Pa s]	Dynamic viscosity
λ	[W/(m K)]	Thermal conductivity
ρ	[kg/m ³]	Density
σ	[N/m]	Surface tension

Indices

'	Liquid
''	Vapour
<i>c</i>	critical value
<i>r</i>	reduced value
<i>i</i>	run index
<i>u</i>	ambient conditions
<i>p</i>	Isobar
<i>v</i>	Isochor
<i>0</i>	ideal gas

2 Introduction

The refrigerant Solkane®404A is a long-term replacement for R502 and R22 in low temperature refrigeration. As R502 consists of 48.8% R22 and 51.2% R115 by weight, its production has been stopped since several years in developed countries¹ because of its content of R115, a chlorofluorocarbon (CFC) with an ozone depletion potential (ODP) of 0.6. The ozone depletion potential of the hydrochlorofluorocarbon (HCFC) R22 is reduced to a fraction of the ODPs of chlorofluorocarbons. R22 is therefore regarded as an intermediate solution. The use of HCFCs will be gradually reduced and these products will finally be banned. By 2030 the production of HCFCs will be phased out in developed countries¹. Accelerated phase out scenarios may apply in selected countries especially in Europe.

Solkane®404A is a near-azeotrope blend with a temperature glide of approx. 0.8 K. It consists of 44 % R125 (CF₃CHF₂), 52 % R143a (CF₃CH₃) and 4 % R134a (CF₃CH₂F) by weight. The hydrofluorocarbons (HFC) R125, R143a and R134a contain only carbon, fluorine and hydrogen. They do not contribute to the depletion of the stratospheric ozone layer. The global warming potential is significantly reduced compared to the CFCs.

Solkane®404A can be used in new equipment and also in retrofitted R502 equipment.

Solkane®404A is non-flammable. Its toxicity is low and comparable to that of R502. The environmental behaviour and the handling of Solkane®404A are described in the material safety data sheet² and in the environmental compatibility brochure³.

¹ In the sense of Montreal Protocol (1995 Vienna meeting)

² Order by Fax : +49 (0) 511 857 2146

³ see Thermodynamics Solkane 507

3 Thermophysical Values

3.1 Physical Data

Chemical name	[-]	Pentafluoroethane/ 1,1,1-Trifluoroethane 1,1,1,2-Tetrafluoroethane
Chemical formula	[-]	CF ₃ CHF ₂ /CF ₃ CH ₃ /CF ₃ CH ₂ F
CAS No.	[-]	150743-07-0
Molecular weight	[kg/kmol]	97.6
Boiling point ¹	[°C]	-46.6
Temperature glide	[K]	0.8
Freezing point ¹	[°C]	-101
Critical temperature	[°C]	72.1
Critical pressure	[bar]	37.4
Saturated liquid density ²	[kg/m ³]	1045
Saturated vapour density ²	[kg/m ³]	65.35
Vapour pressure ²	[bar]	12.45
Enthalpy of vaporization ²	[kJ/kg]	140.1
Liquid thermal conductivity ²	[W/m K]	0.066
Surface tension of liquid ²	[N/m]	4.437 x10 ⁻³
Specific heat capacity of liquid ²	[kJ/(kgK)]	1.541
Specific heat capacity of vapour ²	[kJ/(kgK)]	1.200
Liquid viscosity ²	[Pa s]	0.1245 x10 ⁻³
Saturated vapour viscosity ²	[Pa s]	12.097 x10 ⁻⁶
Flammability limit in air ¹	[Vol.-%]	None ³

¹ at 1.013 bar

² at 25°C and saturated conditions

³ according to DIN 51649 and UL 2128

3.2 Basis of Thermodynamic Calculation

The thermodynamic calculation equations have been adapted to ISO/DIS 17584, as at 12/2003. They fulfil this standard with the exception of the thermal capacities in a saturated state of $0.65 < T_R < 0.95$ and in an overheated state of $0.05\text{MPa} < p < 2.5\text{MPa}$ and $T_{\text{max}} = 475\text{K}$.

The Wagner equation

$$\ln p_R = (A_1(1-T_R) + A_2(1-T_R)^{B_1} + A_3(1-T_R)^{B_2} + A_4(1-T_R)^{B_3} + A_5(1-T_R)^{B_4} + A_6)/T_R \quad (1)$$

where $T_R = \frac{T}{T_c}$ and $p_R = \frac{p}{p_c}$

was chosen to describe the bubble and dew pressures. The constants and values for the critical pressure p_c and the critical temperature T_c are as follows:

	Boiling line	Dew line
A_1 [-]	-7.60299407	-7.81307914
A_2 [-]	3.731263605	4.859254488
A_3 [-]	-7.79162519	-11.0987729
A_4 [-]	11.51536845	16.29371703
A_5 [-]	-9.44588683	-12.3673965
A_6 [-]	0.001223648	-0.00055455
B_1 [-]	1.5	1.5
B_2 [-]	2.0	2.0
B_3 [-]	2.5	2.5
B_4 [-]	3	3
T_c [K]	345.29	
p_c [bar]	37.35	

The density of the boiling liquid is described by the equation

$$\rho'_R = 1 + C_1(1-T_R)^{1/3} + C_2(1-T_R)^{2/3} + C_3(1-T_R) + C_4(1-T_R)^{4/3} \quad (2)$$

where $\rho'_R = \frac{\rho'}{\rho_c}$.

The constants and the value for the critical density are:

C_1 [-]	1.680265	C_4 [-]	0.953230
C_2 [-]	1.410642	ρ_c [kg/m ³]	488.46
C_3 [-]	-1.222830		

The specific heat capacity under ideal gas conditions is represented by the equation

$$c_p^0 = D_1 + D_2T + D_3T^2 + D_4T^3 + D_5/T \quad (3)$$

The coefficients are:

D ₁	[kJ/(kg K)]	2.58689E-01	D ₄	[kJ/(kg K ³)]	-1.18590E-09
D ₂	[kJ/(kg K ²)]	2.24187E-03	D ₅	[kJ/kg]	-4.18094E+00
D ₃	[kJ/kg]	-2.13810E-07			

The equation of state according to Martin-Hou is

$$p = \frac{RT}{z} + \frac{E_1 + F_1T + G_1e^{-kT_R}}{z^2} + \frac{E_2 + F_2T + G_2e^{-kT_R}}{z^3} + \frac{E_3}{z^4} + \frac{E_4 + F_4T + G_4e^{-kT_R}}{z^5} \quad (4)$$

and is a good representation of the pvT relationship for Solkane® 404A. The coefficients of the equation are:

E ₁	[-]	-1.29414E-03	F ₂	[-]	3.10589E-11
E ₂	[-]	6.22058E-07	F ₄	[-]	1.75766E-14
E ₃	[-]	-5.30396E-11	G ₁	[-]	-2.59156E-02
E ₄	[-]	-8.56937E-12	G ₂	[-]	-1.67442E-05
F ₁	[-]	1.89444E-06	G ₄	[-]	7.17681E-10
B	[m ³ /kg]	-3.26856E-04	k	[-]	5.475
R	[bar m ³ /(kgK)]	8.51861E-04			

with $z = v - b$. The equation for specific heat capacity under ideal gas conditions (3) and the thermal equation of state (4) form the basis of the specific enthalpy and entropy calculation.

$$h = H_0 + (pv - RT) + D_1T + D_2 \frac{T^2}{2} + D_3 \frac{T^3}{3} + D_4 \ln T + \frac{E_1}{z} + \frac{E_2}{2z^2} + \frac{E_3}{3z^3} + \frac{E_4}{4z^4} + e^{-kT_R} \cdot (1 + k \cdot T_R) \cdot \left(\frac{G_1}{z} + \frac{G_2}{2z^2} + \frac{G_4}{4z^4} \right) \quad (5)$$

and

$$s = S_0 + R \ln \left(\frac{zp_l}{RT} \right) + D_1 \cdot \ln T + D_2T + D_3 \frac{T^2}{2} - \frac{D_4}{T} - \left(\frac{F_1}{z} + \frac{F_2}{2z^2} + \frac{F_4}{4z^4} \right) + \frac{k}{T_c} e^{-kT_R} \left(\frac{G_1}{z} + \frac{G_2}{2z^2} + \frac{G_4}{4z^4} \right) \quad (6)$$

with $z = v - b$ and $p_f = 1,013 \text{ bar}$.

For the boiling liquid, enthalpy and entropy are calculated with the following equations :

$$h' = J_1 + J_2(1 - T_R) + J_3(1 - T_R)^2 + J_4(1 - T_R)^3 + J_5(1 - T_R)^4 + J_6(1 - T_R)^5 \quad (7)$$

$$s' = 1 + K_1t + K_2t^2 + K_3t^3 + K_4t^4 \quad (8)$$

The temperature t for the calculation of the entropy is in °C and the parameters for both integrated formulas are :

J_1	[-]	325.5684358	J_6	[-]	-13610.9110
J_2	[-]	-892.994422	K_1	[kJ/(kgK ²)]	0.004956173
J_3	[-]	2768.458005	K_2	[kJ/(kgK ³)]	2.40679e-6
J_4	[-]	-9807.73400	K_3	[kJ/(kgK ⁴)]	7.86992e-8
J_5	[-]	18427.02151	K_4	[kJ/(kgK ⁵)]	-5.2699e-10

If neither the kinetic nor the potential energies are taken into account, the specific exergy may be found by the following equation:

$$e = h - h_u - T_u(s - s_u) \quad (9)$$

where the subscript u indicates ambient conditions.

The saturation pressure of the substance at $T_u = 290$ K serves as the reference pressure.

The integration constants h_u and s_u are found by letting

$$h'_{(t=0^\circ\text{C})} = 200.0 \text{ kJ/kg}$$

$$s'_{(t=0^\circ\text{C})} = 1.000 \text{ kJ/(kgK)}$$

$$H_0 = 250.492$$

$$S_0 = -0.269$$

to be

$$h_u = 224.02 \text{ kJ/kg}$$

$$s_u = 1.0832 \text{ kJ/(kg K)}$$

so the specific exergy is $e = 0$ according to existing agreements.

3.3 Transport Properties

3.3.1 Dynamic Viscosity of Saturated Liquid

The viscosity of the saturated liquid of Solkane®404A was measured within the temperature range of -50 to 60 °C. The following regression equation is valid for the liquid phase:

$$\ln\left(\frac{\eta'}{10^{-3}}\right) = L_0 + L_1 t + L_2 t^2 + L_3 t^3 \quad (10)$$

with t in °C and η' in 10^{-3} Pa s. The coefficients are:

$$\begin{array}{ll} L_0 = -1.73999 & [\text{Pa s}] \\ L_1 = -0.013554 & [\text{Pa s/K}] \\ L_2 = -4.7589\text{e-}6 & [\text{Pa s/K}^2] \\ L_3 = -1.0953\text{e-}7 & [\text{Pa s/K}^3] \end{array}$$

Saturated liquid viscosity η' in 10^{-3} Pa s

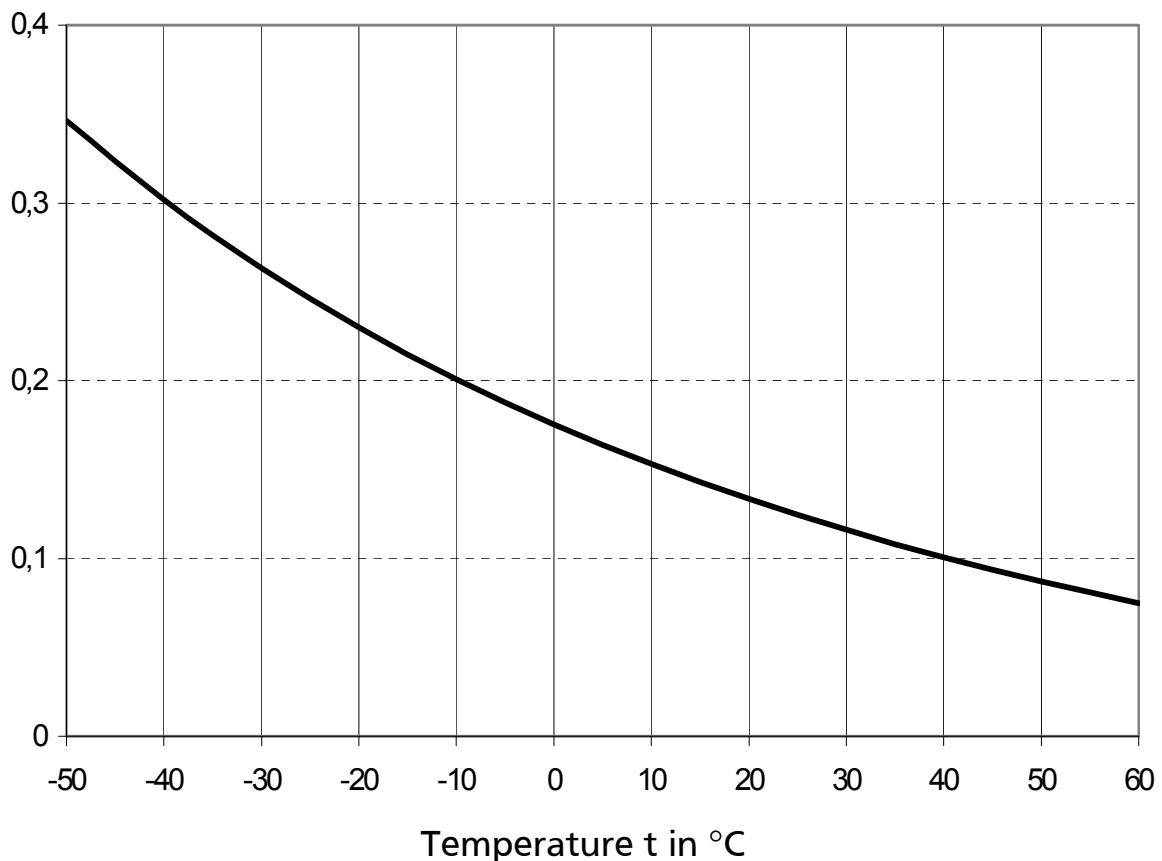


Figure 1: Dynamic viscosity of the saturated liquid

3.3.2 Dynamic Viscosity of Saturated and Superheated Vapour

The viscosity of the saturated and superheated vapour of Solkane®404A was measured in a temperature range of -50 to 50°C. The data can be represented by the following equations

$$\eta = \eta_0 + \Delta\eta \quad (11)$$

with

$$\eta_0 = 2.6696 \times 10^{-2} \times \frac{(MT)^{\frac{1}{2}}}{\sigma^2 \Omega_\eta T^*}, \quad T^* = \frac{kT}{\varepsilon} \text{ and}$$

$$\Omega(T^*) = \exp[0.45667 - 0.53955(\ln(T^*)) + 0.187265(\ln T^*)^2 - 0.03629(\ln T^*)^3 + 0.00241(\ln T^*)^4] \quad (12 \text{ a-c})$$

$$\Delta\eta = T_R^{2.2} \left[\ln(1.65 + \rho_{R0}^{0.8}) \right]^{1.6} \left[e^{\left(1 - \frac{0.78}{T_c}\right) \rho_{r0}} - 1 \right] (F \cdot z_c \cdot \zeta)^{-1}$$

$$z_c = \frac{p_c V_c}{RT_c} \quad \text{and} \quad \rho_{R0} = \frac{\rho - \rho_0}{\rho_c} \quad \text{and} \quad F = 1 \text{ for R404A as a light polar agent.} \quad (12 \text{ d-f})$$

In equation (12) the constants are as follows .

R the universal gas constant	= 8314	[J kmol ⁻¹ K ⁻¹]
ρ_c the critical density	= 484.50	[kg/m ³]
ρ_0 the density at 1.013bar and temperature as defined by T		[kg/m ³]
T_c the critical temperature	= 345.25	[K]

The constants of equation (11) where determined to be

$$\begin{aligned} \zeta &= 42429.18 \text{ [1/(Pa s)]} \\ \sigma &= 0.4968 \text{ [nm]} \\ \varepsilon/k &= 279.31 \text{ [K]} \end{aligned}$$

Saturated vapor viscosity $\epsilon\eta''$ in 10^{-6} Pa s

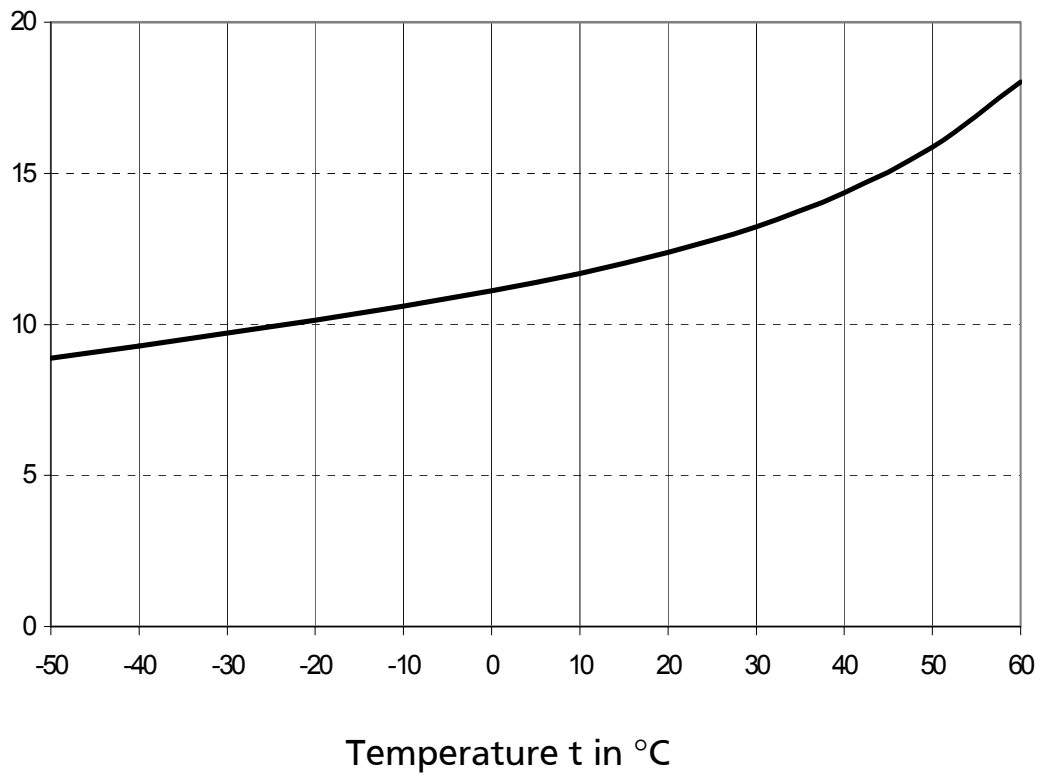


Figure 2: Dynamic viscosity of saturated vapour

3.3.3 Thermal Conductivity of Saturated Liquid

The thermal conductivity of saturated liquid can be expressed with the regression equation

$$\lambda' = M_0 + M_1 t \quad (13)$$

where t is in °C and λ' in $10^{-3}\text{W}/(\text{mK})$. The coefficients of the equation are:

$$M_0 = 76.009 \quad [10^{-3}\text{W}/(\text{mK})] \quad M_1 = -0.4024 \quad [10^{-3}\text{W}/(\text{mK}^2)]$$

Thermal conductivity of saturated liquid λ' in $10^{-3}\text{ W}/(\text{mK})$

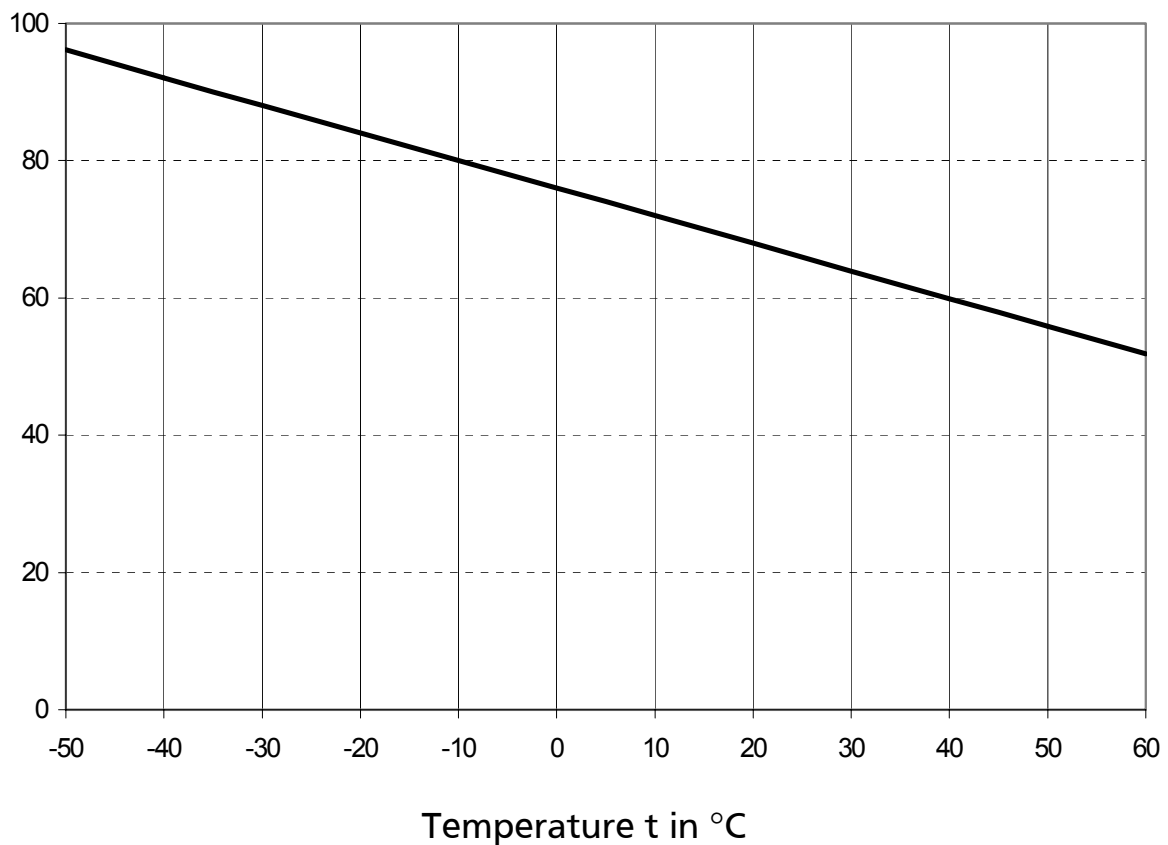


Figure 3: Thermal conductivity of saturated liquid

3.3.4 Thermal Conductivity of Saturated Vapour

The thermal conductivity of saturated vapour can be expressed using the regression equation

$$\lambda'' = N_0 + N_1 t + N_2 t^2 + N_3 t^3 + N_4 t^4 \quad (14)$$

where t is in °C and λ'' in 10^{-3} W/(m K). The coefficients of the equation are as follows:

$N_0 =$	12.709	$[10^{-3}\text{W}/(\text{mK})]$	$N_3 =$	1.0683e-5	$[10^{-3}\text{W}/(\text{m K}^4)]$
$N_1 =$	0.09932	$[10^{-3}\text{W}/(\text{mK}^2)]$	$N_4 =$	5.7339e-8	$[10^{-3}\text{W}/(\text{m K}^5)]$
$N_2 =$	6.2261e-4	$[10^{-3}\text{W}/(\text{mK}^3)]$			

Thermal conductivity of saturated vapour λ'' in 10^{-3} W/(mK)

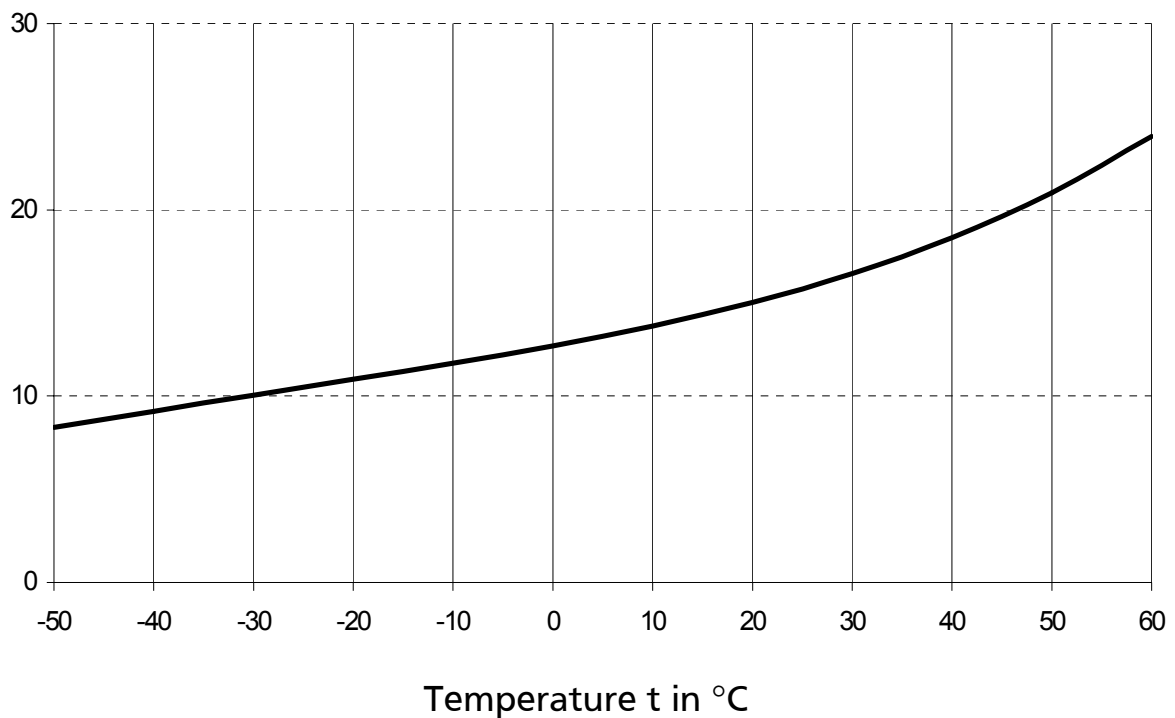


Figure 4: Thermal conductivity of saturated vapour

3.3.5 Surface Tension

The surface tension of the liquid can be expressed using the regression equation

$$\sigma = O_0 + O_1 t + O_2 t^2 + O_3 t^3 \quad (15)$$

where t is in °C and σ in 10^{-3} N/m. The coefficients of the equation are:

$$\begin{array}{llll} O_0 = 7.5370 & [10^{-3}\text{N/m}] & O_2 = 1.6168\text{e-}4 & [10^{-3}\text{N}/(\text{mK}^2)] \\ O_1 = -0.1290 & [10^{-3}\text{N}/(\text{mK})] & O_3 = 1.5624\text{e-}6 & [10^{-3}\text{N}/(\text{mK}^3)] \end{array}$$

Surface tension σ in 10^{-3} N/m

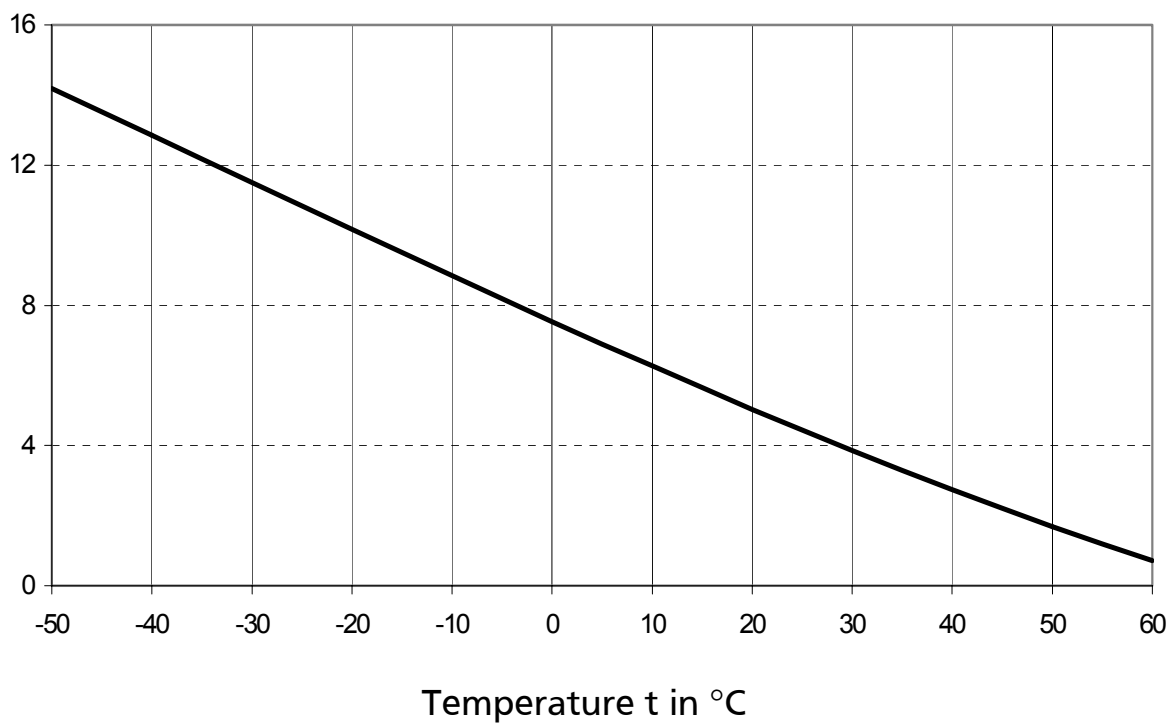


Figure 5: Surface tension

3.3.6 Specific Heat Capacity of Saturated Liquid

The specific heat capacity of saturated liquid can be expressed using the equation

$$c'_p = P_0 + P_1(1-T_R)^{1/9} + P_2(1-T_R)^{2/9} + P_3(1-T_R)^{3/9} + P_4(1-T_R)^{6/9} \quad (16)$$

where $T_R = \frac{T}{T_c}$, c'_p is in kJ/(kg K) and T is in K. The coefficients of the equation are as follows:

$$\begin{aligned} P_0 &= 272.7746241 \text{ [kJ/(kgK)]} & P_3 &= -872.727122 \text{ [kJ/(kgK)]} \\ P_1 &= -1137.19404 \text{ [kJ/(kgK)]} & P_4 &= 72.38836018 \text{ [kJ/(kgK)]} \\ P_2 &= 1666.232657 \text{ [kJ/(kgK)]} \end{aligned}$$

Specific heat capacity of saturated liquid c_p' in kJ/(kgK)

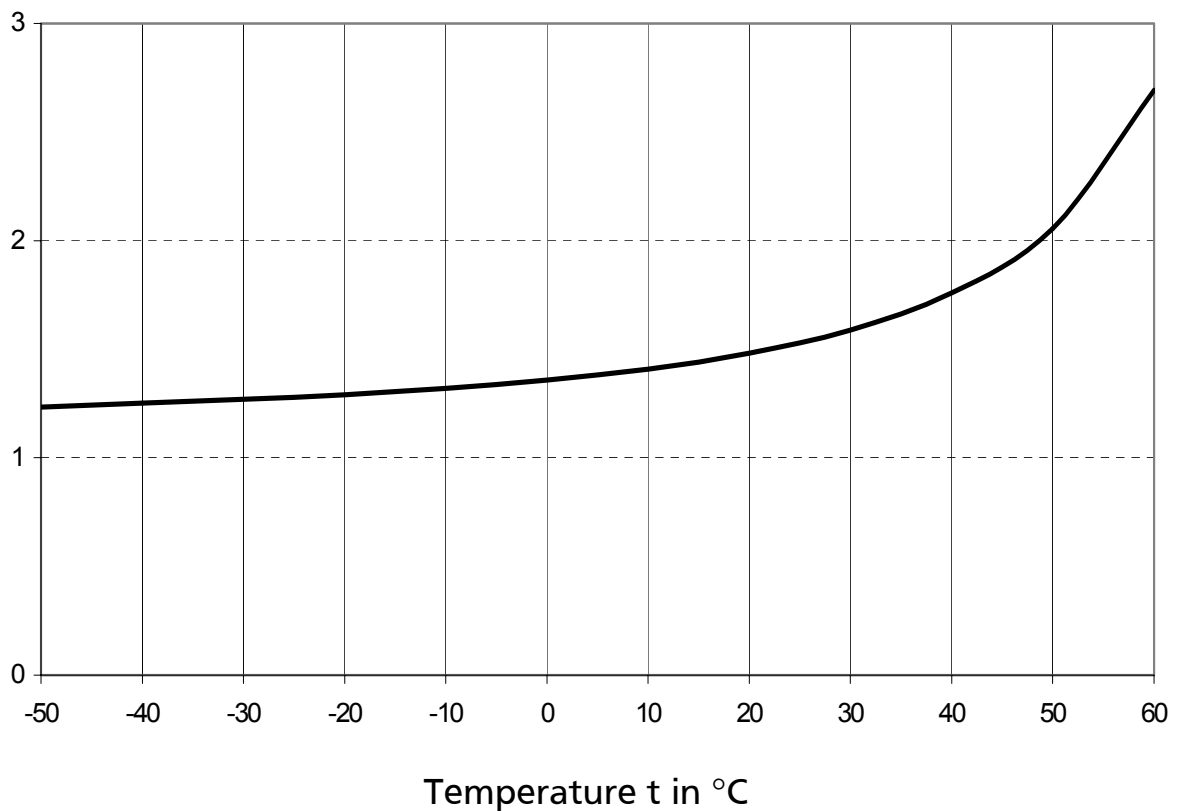


Figure 6: Specific heat capacity of saturated liquid

4 Compatibility of Materials

4.1 Elastomeres

The compatibility of the elastomeres that are normally used in refrigeration systems with Solkane®404A is generally good. Cold extraction tests that were carried out on CR (chlorbutadiene rubber or Neoprene®), NBR (acrylonitrilebutadienerubber) and HNBR (hydrated acrylnitrilbutadiene rubber) showed only slight swelling and yielded negligible amounts of extract. Fluorinated rubbers (FKM and FPM) are not recommended because of their considerable swelling and blistering when used with Solkane®404A or with other HFC refrigerants. Ethylenepropylenediene rubber is only to be recommended where the presence of mineral oil in the refrigeration cycle can be excluded.

The effect of the lubricant that is used must not be ignored. Recommendations made by the lubricant and compressor manufacturers must be followed.

4.2 Thermoplastics

Experience with CFC and HCFC has shown that only a limited number of plastics are resistant to fluorinated refrigerants. Polytetrafluoroethylene, polyacetale and polyamide might be taken into account for the use with Solkane®404A. It is again vital to take the effect of the lubricant into account.

4.3 Metals

Solkane®404A is generally used in conjunction with lubricants (Ester oils, PAG-oils) in refrigeration technology. In combination both materials are compatible with the metals and alloys usually found in machines and apparatus. Only zinc, magnesium, lead and aluminium alloys with more than 2% magnesium by mass should be avoided. The water content of refrigeration oil depending on oil type should especially be taken into account. Values of not more than 50 ppm are to be aimed at.

5 Refrigerant Oils

Like all fluorinated hydrocarbons, Solkane[®]404A is immiscible with mineral oils. Ester oils (POE) are normally used as lubricants. The solubility of these oils in Solkane[®]404A is a function of temperature and composition. The following diagrams show the solubility properties of various lubricants with Solkane[®]404A. Highly viscous lubricants tend to give large miscibility gaps.

The precise miscibility gaps of the individual oils can be obtained from the lubricant manufacturers.

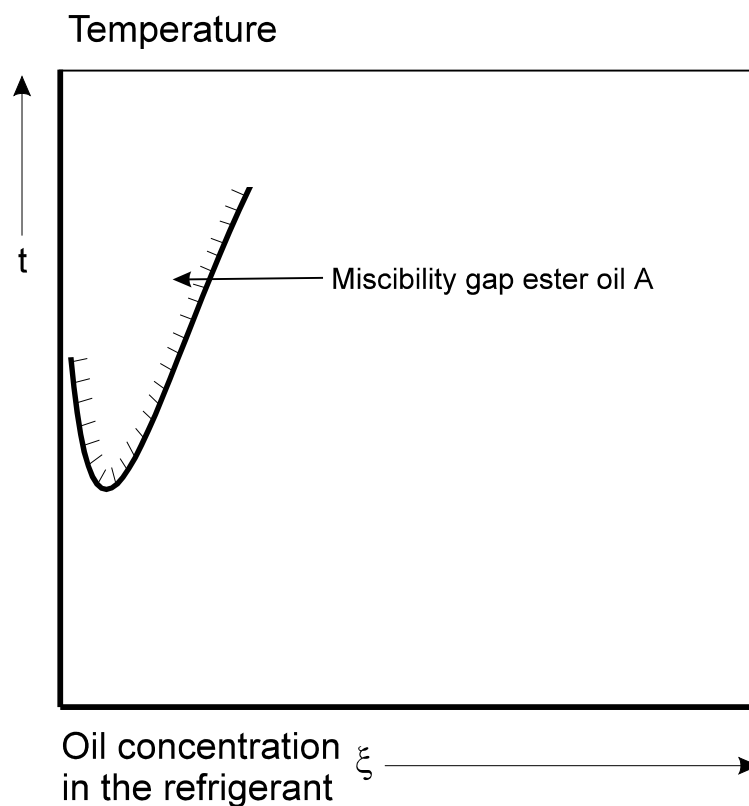


Figure 7: Miscibility behaviour of Solkane[®]404A and ester oil A

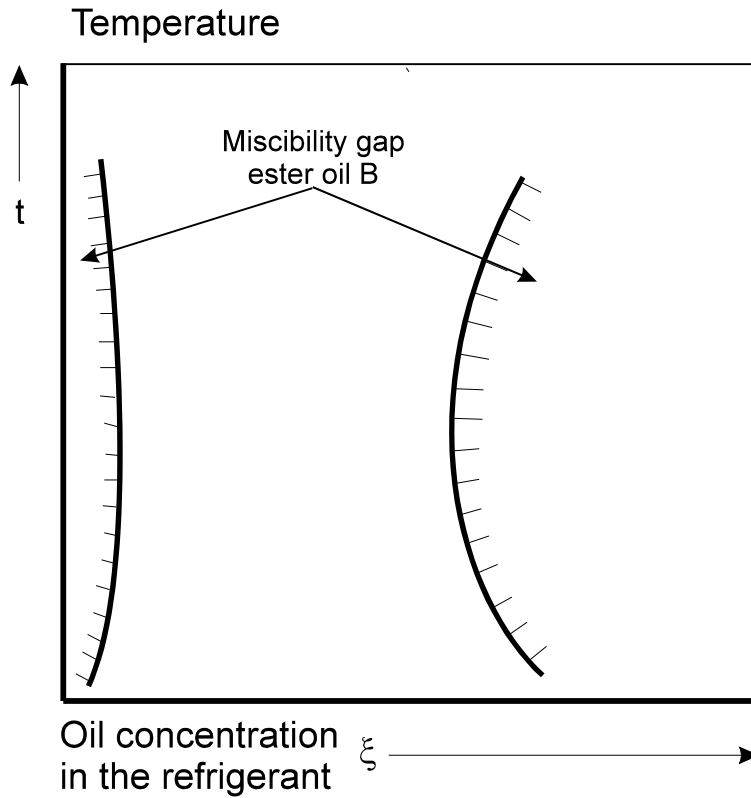


Figure 8: Miscibility behaviour of Solkane®404A and ester oil B

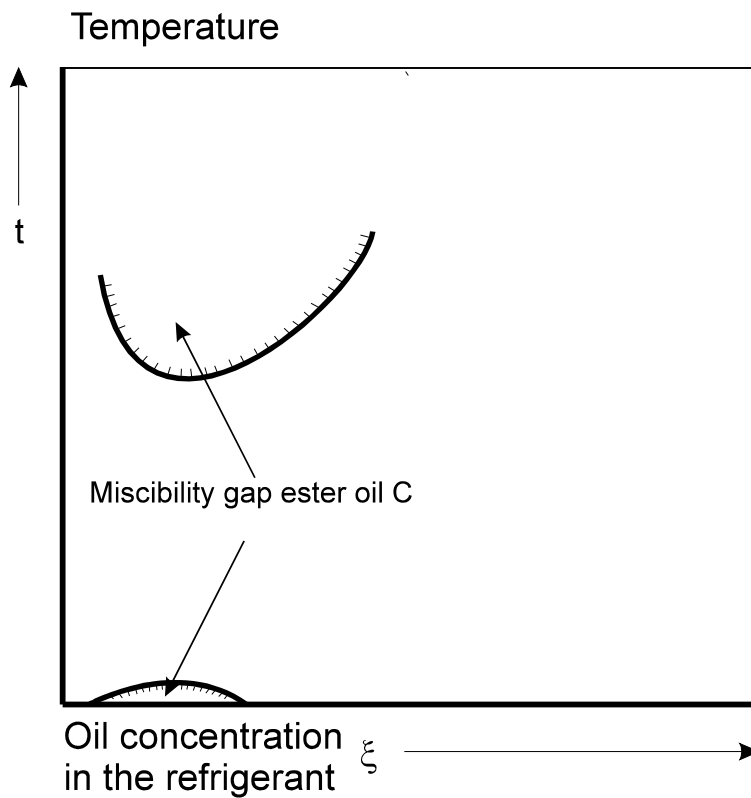


Figure 9: Miscibility behaviour of Solkane®404A and ester oil C

6 Flammability

The explosion limits of R143a are 7.1 - 20.9 % by volume in air. R125 and R134a have no explosion limits. When blended 46/52/4 percent by weight the outcoming mixture has no explosion limits. According to UL 2182 Solkane®404A is non-flammable.

7 Toxicity

The toxicity of R125 and R134a was extensively tested within the scope of the PAFT programme (Programme for Alternative Fluorocarbon Toxicity Testing). PAFT recommended an occupational exposure limit of 1000 ppm for both products. For R143a various manufacturers recommend a maximum exposure limit of 500 ppm related to an eight-hour working day. The toxicity of Solkane®404A can therefore be regarded as low and comparable to the toxicity of R502.

8 Vapour Table, Wet Vapour Range Solkane®404A

t	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
-60	0.508	0.484	0.742	364.71	1.348	2.74	123.10	330.92	207.83	0.6838	1.6644
-59	0.537	0.512	0.743	346.19	1.345	2.89	124.29	331.54	207.25	0.6894	1.6626
-58	0.567	0.541	0.745	328.78	1.342	3.04	125.48	332.15	206.66	0.6951	1.6608
-57	0.598	0.571	0.747	312.43	1.340	3.20	126.68	332.76	206.08	0.7007	1.6590
-56	0.631	0.603	0.748	297.05	1.337	3.37	127.88	333.37	205.49	0.7063	1.6573
-55	0.665	0.636	0.750	282.57	1.334	3.54	129.08	333.98	204.90	0.7119	1.6557
-54	0.700	0.670	0.751	268.94	1.331	3.72	130.28	334.59	204.31	0.7174	1.6540
-53	0.737	0.706	0.753	256.09	1.328	3.90	131.48	335.20	203.71	0.7230	1.6525
-52	0.775	0.743	0.755	243.99	1.325	4.10	132.69	335.81	203.11	0.7286	1.6509
-51	0.815	0.782	0.757	232.57	1.322	4.30	133.90	336.41	202.51	0.7341	1.6494
-50	0.857	0.823	0.758	221.79	1.319	4.51	135.11	337.02	201.91	0.7396	1.6480
-49	0.900	0.865	0.760	211.61	1.316	4.73	136.33	337.62	201.30	0.7451	1.6465
-48	0.945	0.909	0.762	201.99	1.313	4.95	137.55	338.23	200.68	0.7507	1.6452
-47	0.992	0.955	0.764	192.89	1.310	5.18	138.77	338.83	200.06	0.7561	1.6438
-46	1.041	1.002	0.765	184.29	1.307	5.43	139.99	339.43	199.44	0.7616	1.6425
-45	1.091	1.051	0.767	176.15	1.304	5.68	141.22	340.03	198.81	0.7671	1.6412
-44	1.143	1.102	0.769	168.44	1.301	5.94	142.45	340.63	198.18	0.7725	1.6399
-43	1.198	1.155	0.771	161.14	1.297	6.21	143.69	341.23	197.55	0.7780	1.6387
-42	1.254	1.211	0.773	154.22	1.294	6.48	144.92	341.83	196.91	0.7834	1.6375
-41	1.312	1.268	0.774	147.66	1.291	6.77	146.16	342.43	196.26	0.7888	1.6364
-40	1.373	1.327	0.776	141.43	1.288	7.07	147.41	343.02	195.61	0.7942	1.6352
-39	1.435	1.388	0.778	135.52	1.285	7.38	148.66	343.62	194.96	0.7996	1.6341
-38	1.500	1.451	0.780	129.90	1.282	7.70	149.91	344.21	194.30	0.8050	1.6330
-37	1.567	1.517	0.782	124.57	1.279	8.03	151.16	344.80	193.64	0.8103	1.6320
-36	1.636	1.585	0.784	119.50	1.276	8.37	152.42	345.39	192.97	0.8157	1.6310
-35	1.708	1.656	0.786	114.68	1.272	8.72	153.69	345.98	192.29	0.8210	1.6300
-34	1.782	1.728	0.788	110.09	1.269	9.08	154.95	346.56	191.61	0.8263	1.6290
-33	1.858	1.803	0.790	105.73	1.266	9.46	156.22	347.15	190.93	0.8316	1.6280
-32	1.937	1.881	0.792	101.57	1.263	9.85	157.50	347.73	190.24	0.8369	1.6271
-31	2.019	1.961	0.794	97.61	1.260	10.24	158.77	348.31	189.54	0.8422	1.6262
-30	2.103	2.044	0.796	93.83	1.256	10.66	160.06	348.89	188.84	0.8475	1.6253
-29	2.190	2.130	0.798	90.23	1.253	11.08	161.34	349.47	188.13	0.8527	1.6244
-28	2.280	2.218	0.800	86.80	1.250	11.52	162.63	350.05	187.42	0.8579	1.6236
-27	2.372	2.309	0.802	83.53	1.247	11.97	163.92	350.62	186.70	0.8632	1.6228
-26	2.468	2.403	0.804	80.40	1.243	12.44	165.22	351.20	185.98	0.8684	1.6219
-25	2.566	2.500	0.807	77.41	1.240	12.92	166.51	351.77	185.25	0.8736	1.6212
-24	2.667	2.599	0.809	74.56	1.237	13.41	167.82	352.33	184.52	0.8788	1.6204
-23	2.771	2.702	0.811	71.83	1.233	13.92	169.12	352.90	183.78	0.8839	1.6196
-22	2.879	2.808	0.813	69.22	1.230	14.45	170.43	353.47	183.03	0.8891	1.6189
-21	2.989	2.917	0.815	66.73	1.226	14.99	171.74	354.03	182.28	0.8942	1.6182

Vapour Table, Wet Vapour Range Solkane®404A

t	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
-20	3.103	3.029	0.818	64.34	1.223	15.54	173.06	354.59	181.53	0.8994	1.6175
-19	3.220	3.145	0.820	62.06	1.220	16.11	174.38	355.15	180.76	0.9045	1.6168
-18	3.340	3.263	0.822	59.87	1.216	16.70	175.70	355.70	180.00	0.9096	1.6162
-17	3.464	3.386	0.825	57.77	1.213	17.31	177.03	356.25	179.22	0.9147	1.6155
-16	3.591	3.511	0.827	55.77	1.209	17.93	178.36	356.80	178.44	0.9198	1.6149
-15	3.721	3.640	0.829	53.84	1.206	18.57	179.69	357.35	177.66	0.9249	1.6142
-14	3.856	3.773	0.832	51.99	1.202	19.23	181.03	357.90	176.87	0.9299	1.6136
-13	3.994	3.909	0.834	50.22	1.199	19.91	182.37	358.44	176.07	0.9350	1.6130
-12	4.135	4.049	0.837	48.53	1.195	20.61	183.71	358.98	175.27	0.9401	1.6125
-11	4.280	4.193	0.839	46.90	1.192	21.32	185.06	359.52	174.46	0.9451	1.6119
-10	4.430	4.341	0.842	45.33	1.188	22.06	186.41	360.05	173.64	0.9501	1.6113
-9	4.583	4.492	0.844	43.83	1.185	22.82	187.76	360.58	172.82	0.9551	1.6108
-8	4.740	4.647	0.847	42.38	1.181	23.60	189.12	361.11	171.99	0.9602	1.6102
-7	4.901	4.807	0.849	40.99	1.177	24.40	190.48	361.64	171.16	0.9652	1.6097
-6	5.066	4.970	0.852	39.66	1.174	25.22	191.84	362.16	170.32	0.9702	1.6092
-5	5.235	5.138	0.855	38.37	1.170	26.06	193.21	362.68	169.47	0.9751	1.6087
-4	5.409	5.310	0.858	37.14	1.166	26.93	194.58	363.19	168.62	0.9801	1.6082
-3	5.586	5.486	0.860	35.95	1.162	27.82	195.95	363.70	167.76	0.9851	1.6077
-2	5.768	5.667	0.863	34.80	1.159	28.73	197.32	364.21	166.89	0.9901	1.6072
-1	5.955	5.852	0.866	33.70	1.155	29.67	198.70	364.72	166.01	0.9950	1.6067
0	6.146	6.041	0.869	32.64	1.151	30.64	200.00	365.22	165.22	1.0000	1.6062
1	6.342	6.235	0.872	31.62	1.147	31.63	201.47	365.71	164.24	1.0050	1.6058
2	6.542	6.434	0.875	30.63	1.143	32.64	202.86	366.21	163.35	1.0099	1.6053
3	6.747	6.637	0.878	29.68	1.139	33.69	204.25	366.70	162.44	1.0148	1.6049
4	6.957	6.846	0.881	28.77	1.135	34.76	205.65	367.18	161.53	1.0198	1.6044
5	7.171	7.059	0.884	27.88	1.132	35.86	207.05	367.66	160.61	1.0247	1.6040
6	7.391	7.277	0.887	27.03	1.128	36.99	208.46	368.14	159.68	1.0297	1.6035
7	7.615	7.500	0.890	26.21	1.124	38.15	209.86	368.61	158.75	1.0346	1.6031
8	7.845	7.728	0.893	25.41	1.119	39.35	211.28	369.08	157.80	1.0395	1.6027
9	8.080	7.961	0.897	24.65	1.115	40.57	212.69	369.54	156.85	1.0445	1.6022
10	8.320	8.199	0.900	23.91	1.111	41.83	214.11	370.00	155.89	1.0494	1.6018
11	8.565	8.443	0.903	23.19	1.107	43.12	215.54	370.45	154.91	1.0543	1.6014
12	8.815	8.692	0.907	22.50	1.103	44.45	216.97	370.90	153.93	1.0593	1.6009
13	9.071	8.946	0.910	21.83	1.099	45.81	218.40	371.34	152.94	1.0642	1.6005
14	9.333	9.206	0.914	21.18	1.095	47.20	219.84	371.78	151.94	1.0692	1.6000
15	9.600	9.472	0.917	20.56	1.090	48.64	221.28	372.21	150.92	1.0741	1.5996
16	9.873	9.743	0.921	19.95	1.086	50.11	222.73	372.63	149.90	1.0790	1.5992
17	10.15	10.02	0.925	19.37	1.082	51.63	224.19	373.05	148.86	1.0840	1.5987
18	10.44	10.30	0.928	18.80	1.077	53.18	225.65	373.46	147.82	1.0889	1.5983
19	10.73	10.59	0.932	18.25	1.073	54.78	227.11	373.87	146.76	1.0939	1.5978

Vapour Table, Wet Vapour Range Solkane®404A

T	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
20	11.02	10.89	0.936	17.72	1.068	56.43	228.59	374.27	145.68	1.0989	1.5973
21	11.32	11.19	0.940	17.21	1.064	58.11	230.06	374.66	144.60	1.1038	1.5969
22	11.63	11.50	0.944	16.71	1.059	59.85	231.55	375.05	143.50	1.1088	1.5964
23	11.95	11.81	0.948	16.23	1.054	61.63	233.04	375.42	142.38	1.1138	1.5959
24	12.27	12.13	0.953	15.76	1.050	63.46	234.54	375.79	141.25	1.1188	1.5954
25	12.60	12.45	0.957	15.30	1.045	65.35	236.05	376.15	140.11	1.1238	1.5949
26	12.93	12.79	0.961	14.86	1.040	67.28	237.56	376.51	138.95	1.1289	1.5944
27	13.27	13.13	0.966	14.43	1.035	69.28	239.08	376.85	137.77	1.1339	1.5939
28	13.62	13.47	0.970	14.02	1.030	71.33	240.62	377.19	136.57	1.1389	1.5933
29	13.97	13.83	0.975	13.62	1.025	73.44	242.16	377.51	135.36	1.1440	1.5928
30	14.33	14.19	0.980	13.23	1.020	75.61	243.70	377.83	134.13	1.1491	1.5922
31	14.70	14.55	0.985	12.85	1.015	77.84	245.26	378.14	132.87	1.1542	1.5916
32	15.07	14.93	0.990	12.48	1.010	80.14	246.83	378.43	131.60	1.1593	1.5910
33	15.46	15.31	0.995	12.12	1.005	82.52	248.41	378.72	130.31	1.1644	1.5904
34	15.84	15.69	1.000	11.77	1.000	84.96	250.00	378.99	128.99	1.1695	1.5897
35	16.24	16.09	1.006	11.43	0.994	87.48	251.60	379.25	127.65	1.1747	1.5890
36	16.64	16.49	1.011	11.10	0.989	90.08	253.22	379.50	126.29	1.1799	1.5883
37	17.06	16.90	1.017	10.78	0.983	92.75	254.85	379.74	124.90	1.1851	1.5876
38	17.47	17.32	1.023	10.47	0.978	95.52	256.48	379.96	123.48	1.1903	1.5869
39	17.90	17.75	1.029	10.17	0.972	98.37	258.14	380.17	122.03	1.1955	1.5861
40	18.34	18.18	1.035	9.87	0.966	101.32	259.81	380.37	120.56	1.2008	1.5852
41	18.78	18.62	1.042	9.58	0.960	104.37	261.49	380.54	119.06	1.2061	1.5844
42	19.23	19.07	1.048	9.30	0.954	107.52	263.18	380.71	117.52	1.2114	1.5835
43	19.69	19.53	1.055	9.03	0.948	110.78	264.90	380.85	115.95	1.2167	1.5826
44	20.15	20.00	1.062	8.76	0.942	114.16	266.63	380.98	114.35	1.2221	1.5816
45	20.63	20.47	1.069	8.50	0.935	117.66	268.37	381.08	112.71	1.2275	1.5806
46	21.11	20.96	1.077	8.24	0.929	121.29	270.14	381.17	111.03	1.2329	1.5795
47	21.60	21.45	1.085	8.00	0.922	125.06	271.92	381.23	109.31	1.2384	1.5784
48	22.11	21.95	1.093	7.75	0.915	128.97	273.73	381.27	107.55	1.2439	1.5772
49	22.62	22.46	1.101	7.52	0.908	133.04	275.55	381.29	105.74	1.2494	1.5759
50	23.13	22.98	1.110	7.28	0.901	137.27	277.39	381.28	103.89	1.2549	1.5746
51	23.66	23.51	1.119	7.06	0.894	141.69	279.26	381.24	101.98	1.2605	1.5732
52	24.20	24.04	1.129	6.84	0.886	146.29	281.15	381.17	100.02	1.2661	1.5717
53	24.75	24.59	1.139	6.62	0.878	151.11	283.06	381.07	98.01	1.2718	1.5702
54	25.30	25.15	1.149	6.40	0.870	156.15	285.00	380.93	95.93	1.2775	1.5685
55	25.87	25.72	1.160	6.19	0.862	161.44	286.96	380.76	93.79	1.2832	1.5668
56	26.45	26.30	1.172	5.99	0.853	166.99	288.95	380.54	91.59	1.2890	1.5649
57	27.03	26.88	1.184	5.79	0.845	172.85	290.97	380.27	89.31	1.2948	1.5629
58	27.63	27.48	1.197	5.59	0.835	179.03	293.01	379.95	86.94	1.3007	1.5607
59	28.24	28.09	1.211	5.39	0.826	185.58	295.08	379.58	84.50	1.3066	1.5584

Vapour Table, Wet Vapour Range Solkane®404A

T	p'	p''	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kg K]	[kJ/kg K]
60	28.86	28.71	1.226	5.19	0.816	192.55	297.19	379.14	81.95	1.3125	1.5559
61	29.49	29.34	1.242	5.00	0.805	199.99	299.32	378.62	79.30	1.3185	1.5532
62	30.13	29.99	1.259	4.81	0.794	207.99	301.49	378.02	76.53	1.3246	1.5503
63	30.78	30.64	1.278	4.62	0.782	216.63	303.69	377.32	73.63	1.3307	1.5471
64	31.44	31.31	1.299	4.42	0.770	226.04	305.92	376.50	70.58	1.3368	1.5435
65	32.12	31.99	1.323	4.23	0.756	236.39	308.19	375.53	67.34	1.3430	1.5395
66	32.81	32.69	1.349	4.03	0.741	247.95	310.50	374.38	63.88	1.3492	1.5350
67	33.52	33.40	1.379	3.83	0.725	261.10	312.85	372.99	60.14	1.3555	1.5298
68	34.23	34.12	1.415	3.62	0.707	276.49	315.23	371.26	56.03	1.3619	1.5236

Vapour Table, Superheated Range Solkane®404A

20.96 bar 46.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
46	8.24	381.17	1.5795
50	8.71	387.38	1.5988
55	9.23	394.57	1.6209
60	9.69	401.36	1.6414
65	10.12	407.86	1.6608
70	10.52	414.16	1.6793
75	10.90	420.31	1.6971
80	11.26	426.35	1.7143
85	11.61	432.30	1.7311
90	11.94	438.18	1.7474
95	12.27	444.01	1.7633
100	12.58	449.79	1.7789
105	12.89	455.55	1.7942
110	13.19	461.29	1.8093
115	13.48	467.01	1.8242
120	13.77	472.72	1.8388
125	14.05	478.43	1.8532
130	14.33	484.14	1.8674

24.04 bar 52.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
52	6.84	381.17	1.5717
55	7.20	386.52	1.5881
60	7.73	394.54	1.6124
65	8.19	401.90	1.6343
70	8.60	408.83	1.6546
75	8.98	415.48	1.6739
80	9.33	421.92	1.6922
85	9.67	428.20	1.7099
90	9.99	434.37	1.7270
95	10.30	440.44	1.7436
100	10.59	446.44	1.7598
105	10.88	452.39	1.7756
110	11.16	458.29	1.7912
115	11.43	464.16	1.8064
120	11.70	470.01	1.8213
125	11.96	475.84	1.8361
130	12.21	481.66	1.8506
135	12.46	487.47	1.8649

27.48 bar 58.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
58	5.59	379.95	1.5607
60	5.86	384.33	1.5739
65	6.43	393.69	1.6018
70	6.89	401.85	1.6257
75	7.29	409.35	1.6474
80	7.66	416.42	1.6676
85	8.00	423.21	1.6867
90	8.31	429.78	1.7049
95	8.61	436.19	1.7225
100	8.90	442.48	1.7394
105	9.17	448.68	1.7559
110	9.43	454.80	1.7720
115	9.69	460.86	1.7877
120	9.94	466.87	1.8031
125	10.18	472.85	1.8182
130	10.42	478.81	1.8331
135	10.65	484.74	1.8477
140	10.87	490.66	1.8621

21.95 bar 48.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
48	7.75	381.27	1.5772
50	8.00	384.57	1.5874
55	8.54	392.22	1.6109
60	9.02	399.32	1.6324
65	9.45	406.05	1.6524
70	9.85	412.52	1.6714
75	10.23	418.82	1.6896
80	10.59	424.97	1.7072
85	10.93	431.02	1.7242
90	11.26	436.98	1.7407
95	11.57	442.88	1.7569
100	11.88	448.74	1.7727
105	12.18	454.55	1.7881
110	12.47	460.34	1.8033
115	12.76	466.11	1.8183
120	13.04	471.86	1.8330
125	13.31	477.61	1.8476
130	13.58	483.35	1.8619

25.15 bar 54.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
54	6.40	380.93	1.5685
55	6.54	382.89	1.5745
60	7.11	391.68	1.6011
65	7.59	399.49	1.6243
70	8.01	406.73	1.6456
75	8.39	413.61	1.6655
80	8.75	420.23	1.6844
85	9.09	426.65	1.7025
90	9.40	432.94	1.7199
95	9.71	439.11	1.7368
100	10.00	445.20	1.7532
105	10.28	451.22	1.7692
110	10.55	457.19	1.7849
115	10.82	463.12	1.8003
120	11.08	469.02	1.8154
125	11.33	474.89	1.8302
130	11.58	480.75	1.8448
135	11.82	486.60	1.8593

28.71 bar 60.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
60	5.19	379.14	1.5559
65	5.85	390.06	1.5885
70	6.35	398.95	1.6146
75	6.77	406.89	1.6375
80	7.15	414.27	1.6586
85	7.49	421.28	1.6783
90	7.80	428.03	1.6970
95	8.10	434.59	1.7150
100	8.38	441.00	1.7323
105	8.65	447.29	1.7490
110	8.91	453.50	1.7653
115	9.17	459.64	1.7812
120	9.41	465.72	1.7968
125	9.65	471.76	1.8121
130	9.88	477.77	1.8271
135	10.10	483.75	1.8418
140	10.32	489.71	1.8563
145	10.54	495.66	1.8707

22.98 bar 50.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
50	7.28	381.28	1.5746
55	7.87	389.57	1.6001
60	8.36	397.06	1.6227
65	8.81	404.07	1.6436
70	9.21	410.75	1.6632
75	9.59	417.21	1.6819
80	9.95	423.50	1.6998
85	10.28	429.66	1.7172
90	10.61	435.71	1.7340
95	10.92	441.70	1.7503
100	11.22	447.62	1.7663
105	11.51	453.50	1.7819
110	11.80	459.34	1.7973
115	12.08	465.16	1.8124
120	12.35	470.96	1.8272
125	12.62	476.74	1.8418
130	12.88	482.52	1.8563
135	13.14	488.30	1.8705

26.30 bar 56.00°C

<i>t</i>	<i>v</i>	<i>h</i>	<i>s</i>
°C	dm ³ /kg	kJ/kg	kJ/kgK
56	5.99	380.54	1.5649
60	6.49	388.35	1.5885
65	7.00	396.78	1.6136
70	7.44	404.42	1.6360
75	7.83	411.57	1.6567
80	8.19	418.40	1.6762
85	8.53	424.99	1.6947
90	8.85	431.41	1.7125
95	9.15	437.70	1.7297
100	9.43	443.88	1.7464
105	9.71	449.98	1.7627
110	9.98	456.02	1.7785
115	10.24	462.02	1.7941
120	10.49	467.97	1.8093
125	10.74	473.90	1.8243
130	10.98	479.80	1.8390
135	11.22	485.69	1.8535
140	11.45	491.57	1.8679

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